A PASSIVE FACULTATIVE WASTEWATER TREATMENT SYSTEM FOR SINGLE-FAMILY RESIDENTIAL USE

By NovaTec Consultants Inc.

For Denis Barker & Associates Limited

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HOUSING TECHNOLOGY INCENTIVES PROGRAM

A PASSIVE

FACULTATIVE TREATMENT SYSTEM

FOR

SINGLE-FAMILY RESIDENTIAL USE

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ABSTRACT

This paper describes the performance testing of a passive facultative treatment process for onsite treatment of wastewater from a single-family residential dwelling. The intent of the system design was to treat domestic wastewater to comparable quality as would be obtained with conventional, mechanical, secondary biological treatment plants, but in a passive manner. The process was based on the principal of solids separation and extended retention time for anaerobic digestion of biological materials.

The system used two tanks and a solids separating system. Influent was directed through a passive, self-cleaning screen. Solids greater than 3 millimetres in diameter, and approximately 5% of the liquid flow were diverted into a tank dedicated to the storage and passive digestion of solids, while the remainder of the influent that passed through the screen was directed to the liquids retention tank. Supernatant from the solids tank was directed to the liquids tank. The liquids tank utilized inlet piping designed to distribute the flow across the tank cross-section and an underflow clarifying weir.

The system successfully and reliably produced an effluent with a quality such that the total suspended solids (TSS) concentration was comparable to, or better than, effluent produced by conventional secondary treatment plants sized for singlefamily dwellings. The system was not able to reduce biochemical oxygen demand (BOD) concentrations to the same standard.

EXECUTIVE SUMMARY

Present options for the treatment of domestic wastewater generated by single-family dwellings can be grouped into two categories:

- Septic tank treatment
- Mechanical, biological secondary treatment

There is a need to develop alternate methods of obtaining better effluent quality with passive systems. A Passive Facultative Treatment System was developed by D. Barker and Associates, based on the principles of solids separation and extended retention in an attempt to produce effluent quality that would be comparable to secondary biological processes, without the addition of power consuming components.

The treatment system tested was comprised of the following components:

- Influent Sampling Chamber
- Solids Separator
- Solids Digester Tank (Digester)
- Liquids Detention Tank (Clarifier)

Liquid was extracted from the system at various locations in the flow path and tested at an independent laboratory for total and soluble five day Biochemical Oxygen Demand, (BOD), Total Suspended Solids (TSS), Nitrite and Nitrate (combined), Ammonia (NH₃), Total Kjeldahl Nitrogen (TKN), and Fecal Coliform (FC).

BOD removal efficiencies varied from 33% to 74%. The TSS removal efficiencies varied from 6% to 97%.

The prototype system was intended to be an alternative to conventional mechanical biological secondary treatment plants for individual homes. Mechanical systems are expected to achieve a 45 mg/L BOD and 60 mg/L TSS level. The system evaluation showed that the BOD level cannot be achieved, but the TSS level is consistently met or bettered.

The solids separation ability of the system, combined with the systems ability to mitigate hydraulic flushes past the solids retention area, will allow the system to perform better than a conventional septic tank with respect to solids transfer in the treated effluent.

The main potential barrier to use of the passive system in a current residential setting is the additional cost associated with the extra tank needed for the digester assembly. This tank also has to be placed slightly deeper in the ground than a

conventional septic tank to allow for the required vertical drop through the separator. This could be problematic in areas of low topographic relief or areas where there is either shallow rock or high groundwater tables.

The successes of the test system were:

- 1. The system reduced solids transfer to the disposal field.
- 2. The separator was an effective device for the separation of gross solids.
- 3. The inlet piping arrangement in the clarifier distributed flow through a greater cross-section of the tank than a conventional inlet pipe.
- 4. The baffle device in the clarifier effectively reduced the transfer of solids through the system.
- 5. The testing apparatus was convenient and reliable.
- 6. Testing showed that macerating the influent created higher BOD and TSS concentrations in the influent, but the system could reduce the concentrations of both parameters to levels which were comparable for both the unmacerated and macerated influent. Pumping of raw effluent to a treatment system, or use of garburators for kitchen wastes would produce similar impacts which would be effectively processed by the treatment system producing an effluent with a quality similar to that of unmacerated influent treated in the same system.

The failures of the test system were:

- 1. BOD concentrations were not reduced to a level that would qualify the system as an equivalent to a conventional mechanical biological secondary treatment plant.
- 2. The polyethylene tanks used were not suited for underground use.

SOMMAIRE

Le présent document décrit l'essai fonctionnel d'un procédé d'épuration facultatif passif pour l'épuration autonome des eaux usées d'une maison individuelle. Un système a été conçu pour épurer de façon passive les eaux domestiques avec une qualité comparable à celle obtenue par les stations d'épuration secondaires mécaniques et biologiques classiques. Le procédé repose sur la séparation des principales matières solides et la prolongation de la durée de rétention nécessaire à la dégradation des matières organiques par digestion anaérobie.

Le système emploie deux bacs et un séparateur de matières solides. L'influent passe par une grille passive autonettoyante. Les matières solides dépassant 3 millimètres de diamètre et environ 5 p. 100 des liquides sont déversés dans un bac destiné à la retenue et à la digestion passive des matières solides, tandis que le reste de l'influent passant par la grille se dirige vers le bac de rétention des liquides. Le liquide surnageant dans le bac des matières solides se déverse dans le bac des liquides. Le bac des liquides comprend un tuyau d'arrivée qui répartit l'influent en travers du bac et un dispositif d'évacuation du dépôt pour clarifier l'eau du déversoir.

Le système réussit à produire infailliblement un effluent d'une telle qualité que la concentration totale des solides en suspension (TSS) est égale ou inférieure à celle produite par les stations d'épuration secondaires classiques destinées aux maisons individuelles. Cependant, il ne peut pas réduire la demande biochimique en oxygène (DBO) avec autant d'efficacité que ces stations.

RÉSUMÉ

Les options d'épuration des eaux domestiques pour les maisons individuelles se divisent en deux catégories :

- Épuration par fosse septique
 - Épuration secondaire mécanique et biologique

Il faudrait élaborer d'autres méthodes pour obtenir une meilleure qualité d'effluent à l'aide de systèmes passifs. Un système d'épuration facultatif passif a été élaboré par l'entreprise D. Baker and Associates selon les principes de la séparation des matières solides et de la prolongation de la durée de rétention pour produire un effluent de qualité comparable à celui que produisent les procédés biologiques secondaires sans avoir recours à des éléments énergivores.

Le système d'épuration testé renferme les éléments suivants :

- un regard d'échantillonnage de l'influent,
- un séparateur de matières solides,
- un bac destiné à la digestion des matières solides (digesteur),
- un bac destiné à la retenue des liquides (clarificateur).

Un laboratoire de l'extérieur a extrait du liquide du système à divers emplacements du circuit d'écoulement pour tester la demande biochimique totale et soluble en oxygène sur cinq jours (DBO), le total des solides en suspension (TSS), les concentrations en nitrite et en nitrate (combinés) et en ammoniaque (NH₃), l'azote total Kjeldahl (ATK) et les concentrations de coliformes fécaux (CF).

Le rendement d'élimination de la DBO varie de 33 à 74 p. 100 et celui du TSS, de 6 à 97 p. 100.

Le système type a été conçu comme solution de rechange aux stations d'épuration secondaires mécaniques et biologiques classiques pour des maisons individuelles. Avec les systèmes mécaniques, le niveau de la DBO s'élève à 45 mg/L et le niveau de TSS, à 60 mg/L. Notre évaluation a révélé qu'avec le système type, on ne peut pas atteindre ce niveau de DBO, mais on peut toujours atteindre le niveau de TSS et même le dépasser.

Puisque le système peut séparer les matières solides et réduire les chasses hydrauliques sortant de la zone de rétention des matières solides, il surpassera la fosse septique classique pour ce qui est de transférer les solides à l'effluent épuré.

L'obstacle principal empêchant l'adoption du système passif dans les maisons individuelles est le coût additionnel que présente le bac supplémentaire pour le digesteur. En outre, ce bac doit être enterré plus profondément qu'une fosse septique classique pour que la chute verticale vers le séparateur soit adéquate. Cela pourrait créer des problèmes dans les régions de relief émoussé, celles où du roc est près de la surface, ou celles où le niveau de la nappe souterraine est élevé.

Voici les points forts du système d'essai :

- 1. Le système a réduit le transfert de matières solides vers le champ d'épuration.
- 2. Le séparateur s'est avéré efficace pour la séparation des matières solides brutes.
- 3. Le tuyau d'arrivée dans le clarificateur a réparti l'influent sur une plus grande partie transversale du bac que ne l'aurait fait un tuyau d'arrivée classique.
- 4. La chicane du clarificateur a réduit efficacement le transfert de solides dans le système.
- 5. L'appareil d'essai était pratique et fiable.
- 6. L'essai a démontré que les concentrations en DBO et en TSS dans l'influent sont plus élevées si on laisse ce dernier macérer, mais que le système pourrait les réduire à des niveaux comparables à celles qui se trouvent dans l'influent macéré et l'influent non macéré. Le pompage d'effluents bruts vers un système d'épuration ou l'utilisation de broyeurs pour les déchets domestiques pourraient avoir des effets analogues sur les concentrations en DBO et en TSS, qui pourraient être réduites par le système d'épuration pour produire un effluent de la même qualité que l'influent non macéré traité par ce même système.

Voici les lacunes du système d'essai :

- 1. La DBO n'a pas été réduite à un niveau permettant d'affirmer que le système se place au même rang que les stations d'épuration secondaires mécaniques et biologiques classiques.
- 2. Les bacs en polyéthylène utilisés n'étaient pas faits pour être enterrés.

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TABLE OF CONTENTS

ABSTRACT

EXECUTIVE SUMMARY

1.0	INTR	INTRODUCTION						
2.0	PHYS	SICAL	COMPONENTS	2				
	2.1 2.2 2.3 2.4 2.5	INFL SOLI SOLI	ERAL DESCRIPTION UENT SAMPLING CHAMBER DS SEPARATOR DS DIGESTER TANK (DIGESTER) IIDS DETENTION TANK (CLARIFIER)	2 2 3 3 3				
3.0	TEST	ing a	ND ANALYSIS	4				
	3.1 3.2		'ING A ANALYSIS	4 4				
			WATER USE INFLUENT SAMPLING AND ANALYSIS	4 5				
	3.3	EFFL	UENT SAMPLING AND ANALYSIS	5				
		3.3.1	BOD & TSS	5				
			3.3.1.1 BOD REMOVAL EFFICIENCIES 3.3.1.2 TSS REMOVAL EFFICIENCIES 3.3.1.3 IMPACT OF THE DIGESTER	6 7 7				
		3.3.3	NITROGEN FECAL COLIFORM VISUAL OBSERVATIONS	7 8 8				
	3.4 3.5 3.6	APPR	PARISON TO TRADITIONAL SYSTEMS ROPRIATENESS OF THE TESTING ENTIAL BARRIERS TO USE IN CURRENT SETTINGS	9 10 10				
4.0	CON	CLUSI	ONS	11				
	4.1 4.2		CESSES URES	11 11				

APPENDIX 1

1.0 INTRODUCTION

The options for the treatment of domestic wastewater generated by single-family dwellings can be grouped into two categories:

- Septic tank treatment
- Mechanical, secondary biological treatment

The first option is an inexpensive, passive method of treating domestic wastewater prior to ground disposal. As such, the capital construction costs, as well as the operational and maintenance costs are relatively low. These have been the systems of choice in non-sewered areas. The major drawback of these systems is that the level of treatment is relatively low and the effluent still has high levels of Biochemical Oxygen Demand (BOD) and Total Suspended Solids (TSS). Land area requirements for the disposal of effluent from these systems are as much as two to three times greater than those required for the disposal of effluent from a secondary treatment system.

There are several technologies utilized in single-family residential mechanical, secondary biological treatment plants. The majority of these systems can consistently produce effluent with a quality better than 45 mg/L of BOD and 60 mg/L of TSS. These treatment plants are expensive when compared to the septic tank systems and require mechanical components to either drive pumps for fluid transfer, or compressors for air injection. The improved level of treatment permits the use of smaller land areas for the disposal of effluent when compared to land areas required for the disposal of septic tank treated effluent. However, there is an ongoing requirement and associated operational cost for power and maintenance of mechanical treatment plants. In areas where power supply is unavailable or unreliable, and where technical expertise is not available, the mechanical treatment systems are often inappropriate for use. Lands that are suitable for ground disposal of septic tank treated effluent are becoming more scarce. Higher levels of treatment are required to protect human health in areas where the lands are marginally suitable for ground disposal of septic tank treated effluent. A passive system that could produce secondary level quality wastewater would be beneficial to landowners where the ability of the ground to accept wastewater is limited, or where power supply is often interrupted or unreliable.

The objective of the development of the passive treatment system was to achieve a 45 mg/L BOD and 60 mg/L TSS effluent level without utilizing electrical components and power.

2.0 PHYSICAL COMPONENTS

2.1 GENERAL DESCRIPTION

The treatment system that was tested consisted of the following components:

- Influent Sampling Chamber
- Solids Separator
- Solids Digester Tank (Digester)
- Liquids Detention Tank (Clarifier)

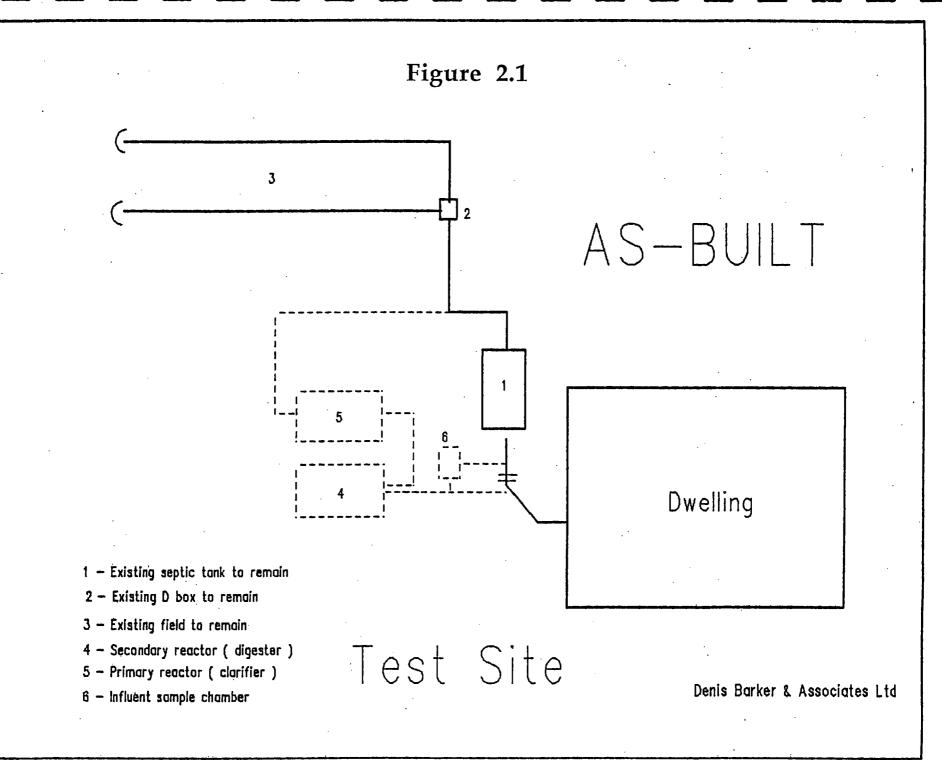
The flow path through the system is shown schematically in Figure 2.1. Raw wastewater originating in the residence was directed to the separator, where solids greater than 3 millimetres (0.125 inches) in diameter were removed from the influent. The solids, along with approximately 5% of the liquid stream, were directed to the solids retention tank. The remainder of the liquid stream was directed to the clarifier and then to the disposal field.

Supernatant overflow from the digester was directed to the clarifier. The general arrangement of the components and the interconnecting piping is also shown in Figure 2.1

A sampling station was installed in an adjacent building. Extraction tubes were installed into the influent sampling chamber, onto both sides of the "bio-brush" in the last chamber of the digester, and onto both sides of the "bio-brush" in the last chamber of the clarifier.

2.2 INFLUENT SAMPLING CHAMBER

The influent sampling chamber was used to take composite samples of the influent sewage, rather than taking grab samples elsewhere in the flow process. A sample was extracted from the chamber, and the remaining contents redirected back to a septic tank not connected to the test treatment system. This was done with a small discharge pump, recirculation piping, and valves. This had the effect of macerating the sewage making it less "separable". In some cases, the macerated influent was then pumped from the septic tank into the test treatment system to test the performance with macerated influent. Before and after the influent was macerated with the transfer pump, composite influent samples were taken to evaluate the impact of maceration on the BOD and TSS concentrations of the influent.



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2.3 SOLIDS SEPARATOR

Influent sewage was passed through a passive self-cleansing separator / screen situated inside the solids digester tank (see Section 2.4). The separator, which had its design optimized before installation, was fitted with a screen capable of separating all solids greater than 3 millimetres (0.125 inches) in diameter from the flow stream. Approximately 5% of the influent liquid, followed the solids stream. Influent passing through the separator was directed to the liquids detention tank (see Section 2.5)

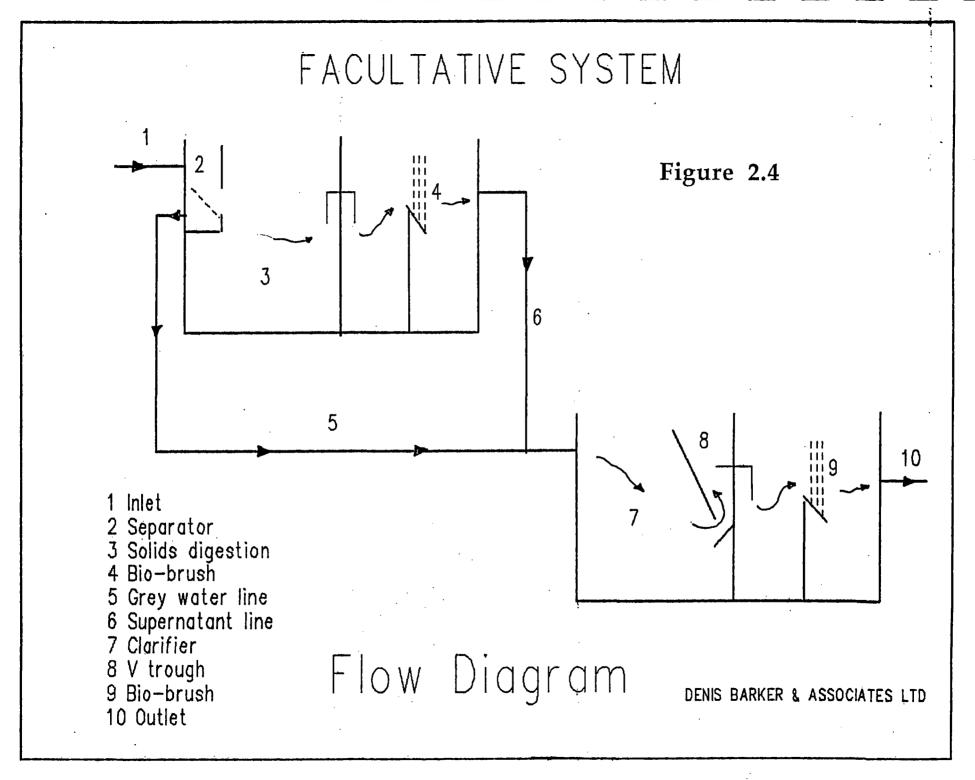
2.4 SOLIDS DIGESTER TANK (DIGESTER)

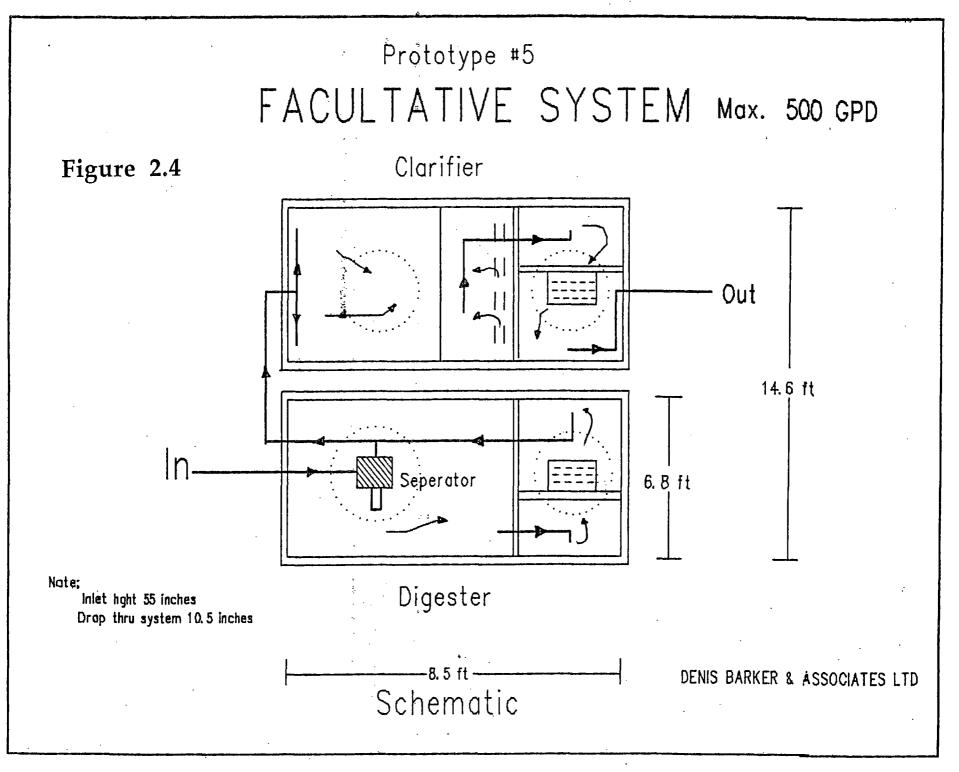
Solids extracted from the influent, and approximately 5% of the influent liquid portion, were directed into the solids digester tank. This tank consisted of two main compartments separated by an internal baffle wall. The second of the two compartments was further subdivided using a non-structural wall for the purposes of liquid separation. In one of these sub-compartments, a fixed-growth bacterial culture was encouraged by mounting a passive media "bio-brush". The tank had an internal capacity of 5,455 litres (1,200 Imperial gallons), but only retained approximately 3,600 litres (800 Imperial gallons) because of the space occupied by the separator. Supernatant from the digester tank was directed to the liquids detention tank. The general arrangement of the tank and piping is shown in Figure 2.4.

2.5 LIQUIDS DETENTION TANK (CLARIFIER)

The influent passing through the solids separator was directed to the liquid detention tank. The configuration of the clarifier was similar to that of the solids digester tank with three exceptions:

- 1. The liquid level was substantially higher. The tank was installed lower than the solids tank to allow gravity drainage from the separator to the normal operating level in the liquids tank.
- 2. To minimize any potential short-circuiting, the influent piping was fitted with a diffuser to spread the flow across the entire tank cross-section.
- 3. The internal baffle in the liquid tank was fitted with a clarifier weir designed to pass liquid from the clearest zone within the tank.





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3.0 TESTING AND ANALYSIS

3.1 TESTING

A sampling schedule was developed at the start of the project to ensure sample acquisition during conditions typical of all four seasons in the Victoria area. All analytical work was completed by JB Laboratories of Victoria, BC, using standard testing protocols.

All scheduled samples were tested for total and soluble five day Biochemical Oxygen Demand (BOD), and Total Suspended Solids (TSS). BOD and TSS are the standard tests used in evaluating treatment system performance. In addition, some samples were tested for Nitrite and Nitrate (combined), Total Kjeldahl Nitrogen (TKN) and Fecal Coliform (FC). The testing reports are enclosed as Appendix 1.

During different days of the week, influent samples were taken from the sampling chamber in both a raw and macerated form. Influent sampling was suspended when analysis indicated a consistency of influent quality (see Section 3.2.2).

Temperatures were measured in the discharge chambers of the clarifier using a mercury thermometer suspended in the liquid. pH was measured using a Hach titration kit, and dissolved oxygen (DO) was measured with a hand-held DO meter. Observations of sludge accumulation in the solids tank were made visually with the aid of a "sludge judge".

The sampling and testing procedure was adequate to evaluate the system for compliance with performance standards for conventional mechanical secondary biological treatment plants.

3.2 DATA ANALYSIS

3.2.1 Water Use

During the test period the residence was occupied by three adults. Water usage was evaluated by recording data from the domestic water meter on a daily basis. The supply line to the house developed a small leak in mid-September. Water use records were suspended at that time. Prior to that date, the total water use averaged 572 litres (126 Imperial gallons) per day or 191 litres (42 Imperial gallons) per person per day.

3.2.2 Influent Sampling And Analysis

Six influent samples were analyzed for total BOD and TSS. Five of the six BOD samples were also analyzed for soluble BOD. In addition, six influent samples were macerated and analyzed for total BOD and TSS. Five of the six macerated samples were also analyzed for soluble BOD. One sample of both the raw and macerated influent was analyzed for combined nitrite (NO_2 -) and nitrate (NO_3 -), Total Kjeldahl Nitrogen (TKN), ammonia (NH_3), and fecal coliform (FC).

The total BOD concentration of the unmacerated influent varied from 67 mg/L to 234 mg/L. The soluble BOD concentration of the unmacerated influent varied from 38 mg/L to 191 mg/L. The total BOD concentrations of the macerated influent samples were higher than those of the raw influent and varied from 133 mg/L to 540 mg/L. The soluble BOD concentrations of the macerated influent samples varied from 36 mg/L to 200 mg/L. This was expected as the surface area of the solids available for biodegradation was increased by the maceration process.

The TSS concentration of the unmacerated influent varied from 32 mg/L to 47 mg/L with the exception of one sample taken on laundry day where the influent TSS was found to be 300 mg/L. The TSS concentrations of the macerated influent varied from 176 mg/L to 510 mg/L. This was again expected as the maceration process decreased the size of the larger particles, but increased the overall surface area and number of smaller particles.

Table 3.2.2, shown on the next page, presents a summary of the data detailed in this section including the mean and median values. The analytical results for nitrogen and fecal coliform are presented and discussed in Sections 3.3.2 and 3.3.3 respectively. Graph 3.2.2, also shown on the next page, presents a graphical summary of this same BOD and TSS data.

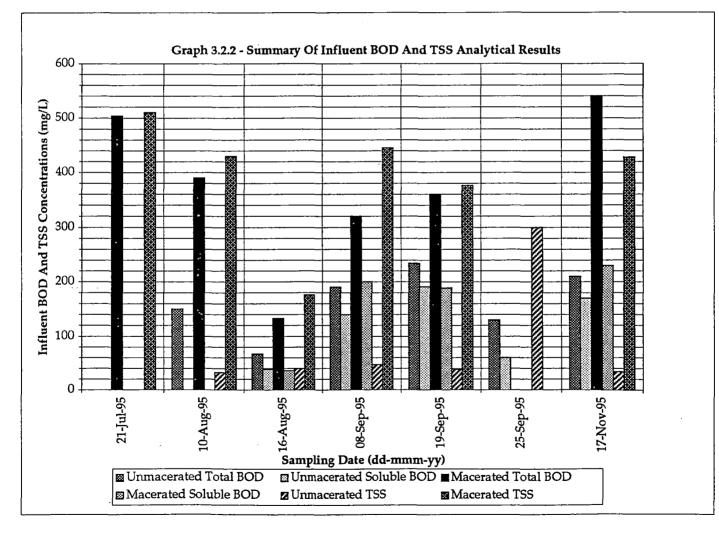
3.3. EFFLUENT SAMPLING AND ANALYSIS

3.3.1 Biochemical Oxygen Demand And Total Suspended Solids

Seventeen samples of effluent from the discharge chamber of the clarifier were analyzed for total BOD and TSS over a six month period beginning in August 1995. Twelve of the seventeen samples were also analyzed for soluble BOD.

September 25, 1995 was a laundry day. In this particular case, effluent sampling was undertaken 24 hours after influent sampling to allow the effects of the "wash day" cycle to manifest themselves in the clarifier sampling results. The total BOD

	Unmacerated	Unmacerated	Macerated	Macerated	Unmacerated	Macerated
Date	Total BOD	Soluble BOD	Total BOD	Soluble BOD	TSS	TSS
(dd-mmm-yy)	(mg/L)	(mg/L)	(mg/L)	(mg/L)	(mg/L)	(mg/L)
21-Jul-95	-	-	504	-	-	510
10-Aug-95	150	-	390	-	32	430
16-Aug-95	67	38	133	36	40	176
08-Sep-95	190	140	320	200	47	445
19-Sep-95	234	191	360	189	38	376
25-Sep-95	130	60	_	-	300	
17-Nov-95	210	170	540	230	34	428
Mean	164	120	375	164	82	394
Median	170	140	375	195	39	429



concentration of the influent sample on September 25, 1995 was the second lowest of the samples, but there was no appreciable difference in the effluent total BOD concentration for this date when compared to the others. The TSS concentration of the influent sample on September 25, 1995 was the highest of the influent samples but the effluent TSS concentration was not appreciably different than that of other samples.

Four of the samples were taken from the chamber ahead of the "bio-brush". The analytical results for these four samples showed that total BOD, TSS, and soluble BOD concentrations were marginally higher than those in the discharge chamber of the clarifier which suggested that the "bio-brush" was acting like a screening device. The brush was devoid of any culture which suggested that it was not supporting any biological activity capable processing organic matter resulting in a lower total BOD concentration in the effluent. It was determined that the effluent in this chamber did not have any dissolved oxygen, so it was not surprising that there was no attached growth.

Near the end of the testing program, a small air pump was added in an attempt to increase the DO concentration in the clarifier. Although a low concentration of DO was detected in the clarified effluent, it was insufficient to support biological activity.

Total BOD concentrations in the clarifier effluent ranged from 37 mg/L to 140 mg/L. Soluble BOD concentration in the clarifier effluent ranged from 26 mg/L to 142 mg/L. The clarifier effluent had a TSS concentration that ranged from 11 mg/L to 46 mg/L.

Table 3.3.1, shown on the next page, presents a summary of the data detailed in this section including the mean and median values. Graph 3.3.1, also shown on the next page, presents a graphical summary of this same BOD and TSS data.

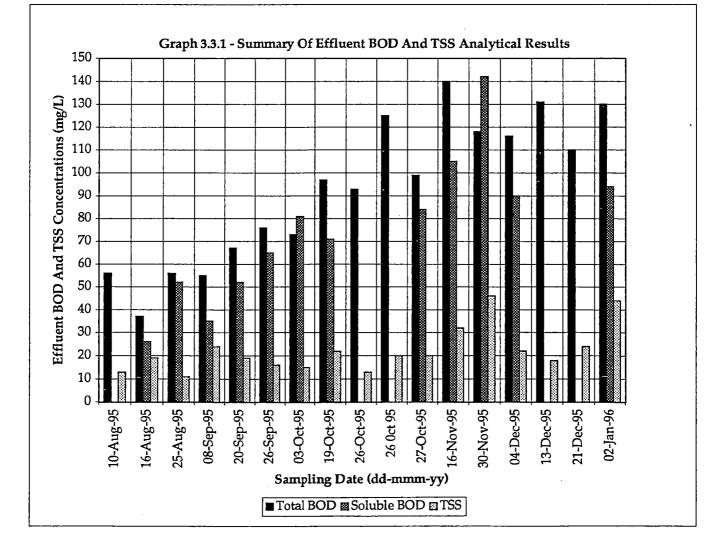
3.3.1.1 BOD Removal Efficiencies

Six samples of influent and clarifier effluent were sampled either on the same day or within twelve hours of each other. The influent and effluent data from these dates is compared in order to determine the overall efficiency of the treatment system. The BOD removal efficiencies are presented on the next page in Table 3.3.1.1 and in Graph 3.3.1.1.

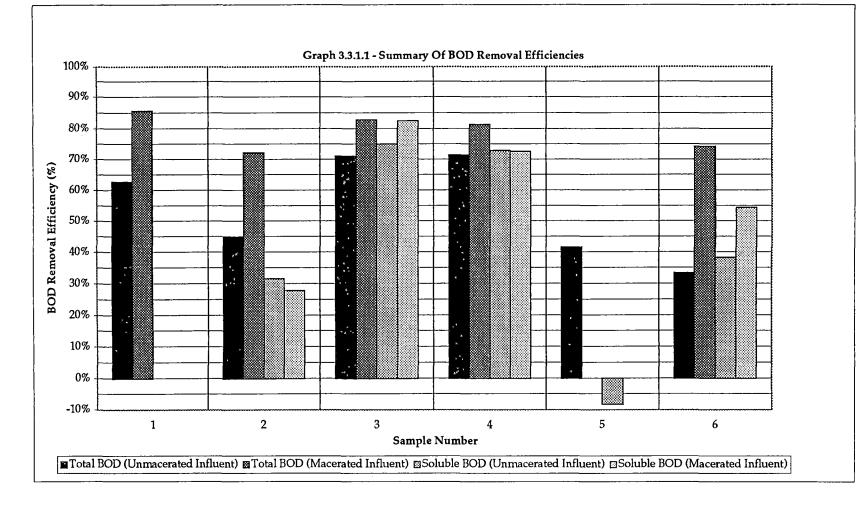
In considering the unmacerated influent, total BOD removal efficiencies varied from 33% to 71% with a mean of 54%. Total BOD removal efficiencies, when considering the macerated influent, varied from 72% to 86% with a mean of 79%.

Table 3.3.1 - Summary Of Effluent BOD And TSS Analytical Results									
Date	Total BOD	Soluble BOD	TSS	Remarks					
(dd-mmm-yy)	(mg/L)	(mg/L)	(mg/L)						
10-Aug-95	56	-	13	-					
16-Aug-95	37	26	19	-					
25-Aug-95	56	52	11	•					
08-Sep-95	55	35	24	-					
20-Sep-95	67	52	19	-					
26-Sep-95	76	65	16	1 Day Lag - Laundry Day					
03-Oct-95	73	81	15	-					
19-Oct-95	97	71	22	-					
26-Oct-95	93	-	13	House Empty					
26 0ct 95	125	-	20	Pre-Bio-Brush, House Empty					
27-Oct-95	99	84	20	Pre-Bio-Brush, House Empty					
16-Nov-95	140	105	32	Pre-Bio-Brush					
30-Nov-95	118	142	46	Pre-Bio-Brush					
04-Dec-95	116	90	22						
13-Dec-95	131	-	18	Post-Air					
21-Dec-95	110	-	24	Post-Air					
02-Jan-96	130	94	44						
Mean	93	75	22	-					
Median	97	76	20						

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Unmacerated	Macerated		Unmacerated	Macerated	Unmacerated	Macerated		Unmacerated	Macerated
Influent	Influent	Effluent	Removal	Removal	Influent	Influent	Effluent	Removal	Removal
Total BOD	Total BOD	Total BOD	Total BOD	Total BOD	Soluble BOD				
(mg/L)	(mg/L)	(mg/L)	(%)	(%)	(mg/L)	(mg/L)	(mg/L)	(%)	(%)
150	390	56	63%	86%	-	-	-	-	-
67	133	37	45%	72%	38	36	26	32%	28%
190	320	55	71%	83%	140	200	35	75%	83%
234	360	67	71%	81%	191	189	52	73%	72%
130	-	76	42%		60	-	65	-8%	-
210	540	140	33%	74%	170	230	105	38%	54%
		Mean	54%	79%			Mean	42%	59%
		Median	54%	81%			Median	38%	63%



Soluble BOD removal efficiencies for the unmacerated influent ranged from -8% to 75% with a mean of 42%. No explanation for the negative removal efficiency can be given other than human sampling error. The macerated influent soluble BOD removal efficiency ranged from 28% to 83% with a mean of 59%.

3.3.1.2 TSS Removal Efficiencies

The TSS removal efficiencies are presented on the next page in Table 3.3.1.2 and in Graph 3.3.1.2. In considering the unmacerated influent, TSS removal efficiencies varied from 6% to 95% with a mean of 52%. The TSS removal efficiencies for the macerated influent ranged from 89% to 97% with a mean of 94%.

3.3.1.3 Impact Of The Digester

Six samples of effluent from the digester and the clarifier were sampled on the same day in order to determine the how the digester and clarifier components were functioning relative to each other. The samples were analyzed for total and soluble BOD, and TSS.

The results, presented in Table 3.3.1.3 and in Graphs 3.3.1.3a, b, and c, indicate that the total and soluble BOD concentrations of the samples from both the digester and the clarifier rose proportionately, until mid-September. The clarifier effluent had higher total and soluble BOD concentrations than the digester effluent until this time. In mid-September and at later dates, the clarifier effluent was found to have lower total and soluble BOD concentrations than the digester effluent.

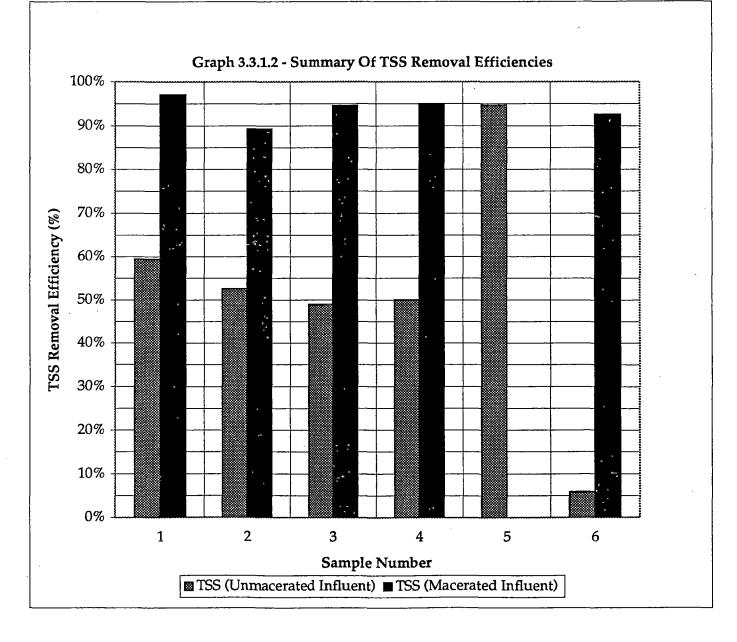
The TSS concentrations were consistently higher in the digester effluent than in the clarifier effluent for all samples taken after September 8, 1995. The last comparative sample taken on November 16, 1995 indicated that the TSS concentration of the clarifier effluent was only marginally lower than that of the digester samples. The configuration of the settling weir in the clarifier is anticipated to encourage better settling of solids at all times. Any carryover of solids from the digester was expected to be reduced as the supernatant flows through the clarifier.

3.3.2 Nitrogen

One effluent sample was tested for nitrite, nitrate, and ammonia in October, 1995. One sample of influent and one of effluent were analyzed in November, 1995 to determine nitrogen removal efficiencies. The November samples were tested for nitrite, nitrate, ammonia, and TKN. There was no appreciable difference in nitrite and nitrate concentrations, but the ammonia concentration in the effluent increased

Unmacerated	Macerated		Unmacerated	Macerated
Influent	Influent	Effluent	Removal	Removal
TSS	TSS	TSS	TSS	TSS
(mg/L)	(mg/L)	(mg/L)	(%)	(%)
32	430	13	59%	97%
40	176	19	53%	89%
47	445	24	49%	95%
38	376	19	50%	95%
300	-	16	95%	-
34	428	32	6%	93%
		Mean	52%	94%
		Median	51%	95%

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		Digester		Clarifier			
Date	Total BOD	Soluble BOD	TSS	Total BOD	Soluble BOD	TSS	
dd-mmm-yy)	(mg/L)	(mg/L)	(mg/L)	(mg/L)	(mg/L)	(mg/L)	
16-Aug-95	20	12	10	37	26	19	
08-Sep-95	26	17	25	55	35	24	
20-Sep-95	35	24	30	67	52	19	
26-Sep-95	100	95	26	76	65	16	
03-Oct-95	106	86	25	73	81	15	
16-Nov-95	140	-	34	140	105	32	

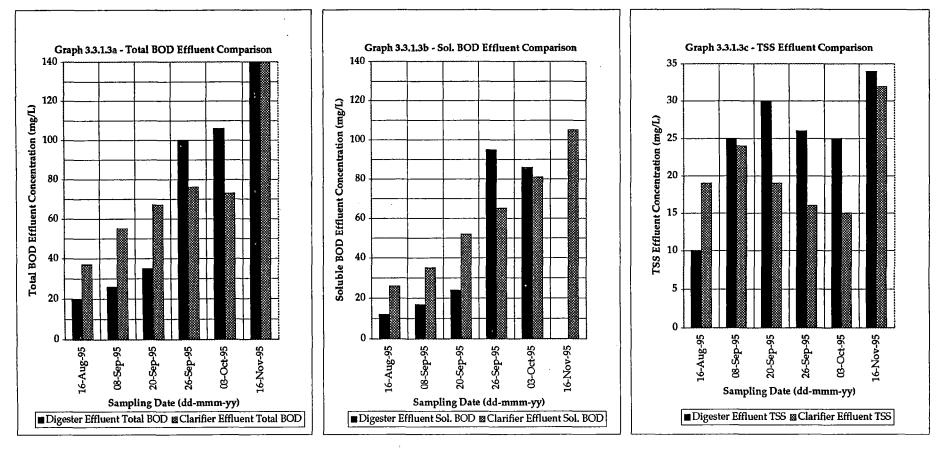


Table 3.3.2 - Summary Of Nitrogen Analytical Results										
Date	NO ₂ -, NO ₃ -	NH ₃	TKN							
(dd-mmm-yy)	(mg/L)	(mg/L)	(mg/L)							
19-Oct-95 (effluent)	0.050	62.4	-							
17-Nov-95 (influent)	0.003	34.6	122							
16-Nov-95 (effluent)	0.004	59.6	70.4							

by 72% while the TKN concentration in the effluent decreased by 54%. Table 3.3.2 presents a summary of the nitrogen data.

3.3.3 Fecal Coliform

Samples were analyzed for fecal coliform reduction during the November testing program. The system generally provided a one-log reduction in fecal coliform concentrations, from 2,200,000 CFU per 100 millilitres in the influent to 390,000 CFU per 100 millilitres in the effluent.

3.3.4 Visual Observations

The system was installed in early July, 1995 and the digester did not overflow until August. The digester was visually inspected several times during this period. The solids level was evaluated with a "sludge judge", the temperature of the clarifier was recorded at random times throughout the testing program, and general appearances were observed.

Neither the solids retention tank, nor the clarifier developed a "scum blanket" typical of a septic tank installation. The solids in the first chamber of the solids tank, did not turn black which would have indicated an absence of anaerobic activity in this cell. In the second cells, black bacteria were noted indicating that septic activity was occurring in the last cell of the digester. The sludge buildup in the solids tank over the course of the testing was less than 300 millimetres.

The temperature in the last compartment of the clarifier was 22.2 °C in July, falling to 20.0 °C on September 8, 17.8 °C on September 17, and 13.3 °C on November 30, 1995. The performance of the system was not noticeably affected by the temperature.

The test tanks were fabricated from polypropylene. These tanks were supposedly designed for underground installation. Even though the installation was only marginally below the ground surface (approximately 0.2 metres) the tanks suffered considerable distortion due to active earth pressure. Within one month of installation, it was impossible to seal the access manholes. By the end of the test period, the distortion was so severe that the differential displacement across the top of the inspection manholes was in the order of 50 millimetres. The polypropylene tanks were removed and replaced with concrete tanks at the end of the test program.

The system was noted to produce a sewage related odour in the immediate vicinity of the tanks. The smell was not septic, nor typical "sewage odour" but was similar to an ammonia / detergent odour. This condition was aggravated by the inability to seal the access ports of the test tankage. Odours are not expected to be detected from a properly sealed, buried installation.

The ground disposal system at the test site was quite small. The location of the gravity distribution piping was evident as a lush green grass cover grew immediately over the trench surfaces. Within weeks of the installation of the test system, the grass cover over the disposal piping trenches was the same as elsewhere in the yard. The reduction in "green area" could have been a result of the larger retention volume of the new system, or more likely, a reduction in transfer of TSS and BOD associated with instantaneous peak flows that will occur with a conventional septic tank system.

3.4 COMPARISON TO TRADITIONAL SYSTEMS

The prototype system was intended to be an alternative to conventional mechanical biological secondary treatment plants for individual homes. Mechanical systems are expected to achieve a BOD concentration of 45 mg/L and a TSS concentration of 60 mg/L. The system evaluation shows that the BOD level could not be achieved, but the TSS level was consistently met and bettered.

The analysis of the BOD concentrations in the digester and the clarifier indicate that the BOD levels in the effluent can be expected to continue to rise to ultimately match the BOD of the influent (unmacerated).

The passive system performed better than a conventional septic tank treatment system. The separator directed the majority of the gross solids to the digester. The "re-suspension" of solids, and the flushing of BOD through the system was minimized. A more consistent effluent quality is expected from a passive system with the noted configuration than from a conventional septic tank system.

3.5 APPROPRIATENESS OF THE TESTING

The sampling frequency and testing parameters were considered adequate to assess the performance of the system.

The installation was relatively straight forward and can be performed by anyone knowledgeable in the installation of conventional septic tanks. Maintenance of this type of passive system is expected to be comparable to that of a conventional septic tank treatment system.

The test system complies with Provincial standards and regulations pertinent to septic tank systems.

3.6 POTENTIAL BARRIERS TO USE IN CURRENT RESIDENTIAL SETTINGS

The main potential barrier to use of the passive system in a current residential setting is the additional cost associated with the extra tanks needed for the digester assembly. These tanks also have to be placed slightly deeper in the ground than a conventional septic tank to allow for the required vertical drop through the separator. This could be problematic in areas of low topographic relief or areas where there is either shallow rock or high groundwater tables.

4.0 CONCLUSIONS

4.1 SUCCESSES

The successes of the test system were:

- 1. The system reduced solids transfer to the disposal field.
- 2. The separator was an effective device for the separation of gross solids.
- 3. The inlet piping arrangement in the clarifier distributed flow through a greater cross-section of the tank than a conventional inlet pipe.
- 4. The baffle device in the clarifier effectively reduced the transfer of solids through the system.
- 5. The testing apparatus was convenient and reliable.
- 6. Testing showed that macerating the influent created higher BOD and TSS concentrations in the influent, but the system could reduce the concentrations of both parameters to levels which were comparable for both the unmacerated and macerated influent. Pumping of raw effluent to a treatment system, or use of garburators for kitchen wastes would produce similar impacts which would be effectively processed by the treatment system producing an effluent with a quality similar to that of unmacerated influent treated in the same system.

4.2 FAILURES

The failures of the test system were:

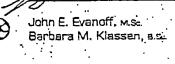
- 1. BOD concentrations were not reduced to a level that would qualify the system as an equivalent to a conventional mechanical biological secondary treatment plant.
- 2. The polyethylene tanks used were not suited for underground use.

Appendix 1

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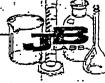
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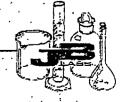
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	#201 - 2840 Nanaimo St. Victoria, B.C.
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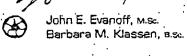
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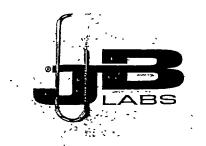


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JOB NO: LR NO:

JB 1624V 20187

See Below

SAMPLING AGENT:

SAMPLING DATE: Client

The sample(s) submitted by the agent have been tested as requested and we report as follows.

Attn: Ivo Van Bastelaere

NovaTec Consultants Inc.

#201 - 2840 Nanaimo St.

August 30, 1995

Victoria, B.C.

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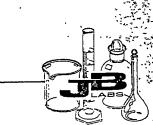
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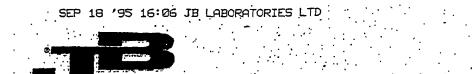
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John E. Evanoff, Misc Barbara M Klassen, esc Analysis performed according to "A Laboratory Manual for the Chemical Analysis of water, Wastewaters and Biological Tissues", Chemistry Laboratory Water Resource Service and/or "Standard Methods/Water and Wastewater", American Public Health Association

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	#201 - 2840 Nanaimo St. Victoria, B.C. V87 4W9
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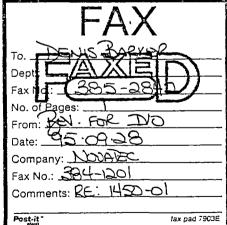
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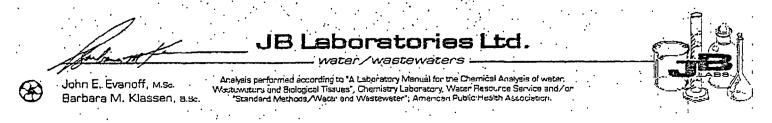
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DATE:	September 28, 1995 LA NO: 20450
	SAMPLINGDATE: See Below
CLIENT:	NovaTec Consultants Inc. SAMPLING AGENT: Client.   #201 - 2840 Nanaimo St. The sample(s) submitted Dythe sgenchave been   Victoria, B.C. Dythe sgenchave been Dythe sgenchave been   V8T 4W9 We report as follows: Dythe second
	Attn: Ivo Van Bastelaere
SAMPLE;	Sample # 1: Macerated Influent. Sep 8/95 Sample # 2: Influent Sample # 3: Clarifier Sample # 4: Digestor
	Sample # 5: Macerated Influent Sep 19/95 Sample # 4: Influent Sample # 7: Clarifier Sep 20/95

· · · ·	•	Sample 1	Sample 2	Sample 3	<u>Sample 4</u>	
Tot Suspended Solids	mq/L	· 445 ·	47 . `	24 .	· 25	•
BOD5 .	mg/L	320	- 190	55	26	:
BOOs, Soluble	mg/L	200	140	- 35	17	· .
					_	•
		<u>Sample S</u>	Sample 6	<u>Sample 7</u>	<u>Sample 8</u>	
. Tot Suspended Solids	mg/L .	376	38 .	. 19	30 ·	
BODs	mg/L	360	234	67 ° .	35	
BÓDs, Soluble	mg/L	189;	• 191,.	52 .	24	۰ ۱۰

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	ABS	·			VICTOR Tel: (60	HD-( RT STREET, IA, B.C. VBW 1H6 4] 385-6112 04] 382-6364	
DATE: -	October 2,	1995			JOB NO: LR NO:	JB 1624V 20450	
CLIENT [.]	• • • • • • •	onsultants Inc. 40 Nanaimo St. B.C.		SAMPLII The sampl by the ag tested as	LING DATE. NG AGENT. le(s) submitted gent have been requested and poort as follows	See Below Client	
SAMPLE.	Sample # Sample # Sample # Sample # Sample # Sample # Sample # Sample # Sample #	Van Bastelaere 1: Macerated I 2: Influent 3: Clarifier 4: Digester 5: Macerated I 6: Influent 7: Clarifier 8: Digester 9: Laundry (In 10: Clarifier 11: Digester	nfluent Se Sep 20/95	限制 9 8/95 9 19/95 9 25/95	GEIVED (	OCT <b>3 1995</b>	
Tot Suspe BODs BODs, Sol	nded Solids uble	mg/L mg/L mg/L	<u>Sample 1</u> 445 320 200	<u>Sample 2</u> 47 190 140	<u>Sample 3</u> 24 55 35	<u>Sample 4</u> 25 26 17	
Tot Suspe BODs BODs, Sol	nded Solids uble	mg/L mg/L mg/L	<u>Sample 5</u> 376 360 189	<u>Sample 6</u> 38 234 191	<u>Sample 7</u> 19 67 52	<u>Sample 8</u> 30 35 24	، مربع م
Tot Suspe BODs BODs, Sol	nded Solids uble	mg/L mg/L mg/L	<u>Sample 9</u> 300 130 60	<u>Sample 10</u> 16 76 65	<u>Sample 11</u> 26 100 95	<u>.</u>	

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John E Evanoff, м se

Barbara M. Klassen, a sc

## JB Laboratories Ltd.

- water/wastewaters _

Analysis performed according to "A Laboratory Manual for the Chemical Analysis of water Wastewaters and Biological Tissues" Chemistry Laboratory Water Resource Service and/or "Standard Methods/Water and Wastewater" American Public Health Assoc at on

P.1 7 FORT STREET. CTORIA, B.C. V8W 1H6 Tel: (604) 385-6112 Fax: (604) 382-6354 JOB NO: JB 1624V LF NO: 20450 SAMPLING DATE: See Below SAMPLING AGENT: Client The sampla(s) submitted by the agent have been beggent have been beggent as follows: p 8/95 p 19/95
, STORIA, B.C. VEW 1H6 Tel: (604) 385-6112 Fax: (604) 382-6354 JOB ND: JB 1624V LR ND: 20450 SAMPLING DATE: See Below SAMPLING AGENT: Client The sample(s) submitted by the agent have been tested has requested and wareport as follows: p 19/75
Tei: (604) 385-6112 Fax: (604) 382-6354 JOB NO: JB 1624V LER NO: 20450 SAMPLING DATE: See Below SAMPLING AGENT: Client The sample(s) submitted by the agent have been tested os requested and wareport as follows: p 8/95
JOB NO: JB 1624V LR ND: 20450 SAMPLING DATE: See Below SAMPLING AGENT: Client The sample(s) submitted by the agent have been Mereport as follows: p 8/95 p 19/95
LE ND: 20450 SAMPLING DATE: See Below SAMPLING AGENT: Client The sample(s) submitted by the agent have been baten has requested and we report as follows: p 8/95
LE ND: 20450 SAMPLING DATE: See Below SAMPLING AGENT: Client The sample(s) submitted by the agent have been baten has requested and we report as follows: p 8/95
LE ND: 20450 SAMPLING DATE: See Below SAMPLING AGENT: Client The sample(s) submitted by the agent have been baten has requested and we report as follows: p 8/95
SAMPLING DATE: See Below SAMPLING AGENT: Client The sample(s) submitted by the agent have been tested as requested and we report as follows: p 8/95
p 8/95
SAMPLING AGENT: Client The sample(a) submitted by the agent have been tested has requested and we report as follows: p 8/95 p 19/95
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Sample 2 Sample 3 Sample 4
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190 55 26
140 35 17
Sample 6 Sample 7 Sample 8
38 19 30 ·
234 67 35
191 52 24
Sample 10 Sample 11
16 26
76 100
65 95
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LADS			04)382-6364
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DATE: October 10	, 1995	JOB NO;	JB. 1624U
		LA NO:	20582
		SAMPLING DATE:	See Below
CLIENT: NousTee C	· · · · · · · · · · · · · · · · · · ·	SAMPLING AGENT.	· • • • • • • • • • • • • • • • • • • •
inovalet u	insultants Inc.	The sample(s) submitted	Client
#201 - 28 Victoria,	10 Nanaimo St.	by the agent have brien	• . :
VICLUIIA,		tested as requested and we report as follows	· · ·
V01 4W7			, .
Attn: Tun	Van Bastelaere		• • • • • • • • • • • • • • • • • • • •
100110 110			
SAMPLE: Sample #	1: Alderly - Clarifier Oct 3/	95	
	2: Alderly - Digester		
	Sample 1 Samp	<u>le 2</u>	
Tot Suspended Solids		,	•
800s	mg/L 73 106		
BODs, Soluble	mg/L 81 86		

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John E. Evanoff, M.S. Barbara M. Klassen, a.sc. 

Analysis performed according to "A Laboratory Manual for the Chemical Analysia of watar, Westewatere and Biological Tissues", Chemistry Laboratory, Water Resource Service and/or "Standard Mathods/Water and Wastewater", American Public Health Association.

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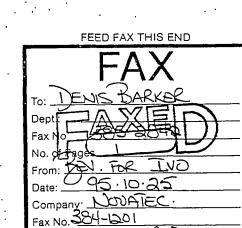
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OCT 25 '95 11:32 JB LABORATORIES LTD	P.2 827 FORT STREET, VICTORIA, B.C. VBW 1H6 Tel: (604) 385-6112 Fax: (604) 382-6364
DATE: October 25, 1995	JOB NO: JB 1624V LR NO: 20582
	SAMPLING DATE: See Below
CLIENT: NovaTec Consultants Inc. #201 - 2840 Nanaimo St.	SAMPLING AGENT: Client
Victoria, B.C. V8T 4W9	by the Agent have been tested as requested and we report as follows:
SAMPLE: Sample # 1. Alderly Classification	
Sample # 1: Alderly - Clarifier . Occ Sample # 2: Alderly - Digester	
Sample # 3: Alderly - Clarifier . Oct	19/95

		. •		Samp]	e 1 .	Sample 2	Sample 3	,
	Tot Suspended Solids	mg/L		. 15	• • •	25	. 22	
	BODș	mg/L		· [·] 73		106	. 97	• •
	BODs, Soluble	mg/L	•••	· 81	·. · ·	86	71	: .
	Nitrite + Nitrate	mg/LN	•				0.050	-
• • •	Ammonia	mg/LN	•		• .	,	. 62.4	
	Faecal Coliform	CFU/100ml	• •	· ·	•		5.7x104	
•				•	:		. :	·

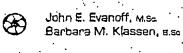


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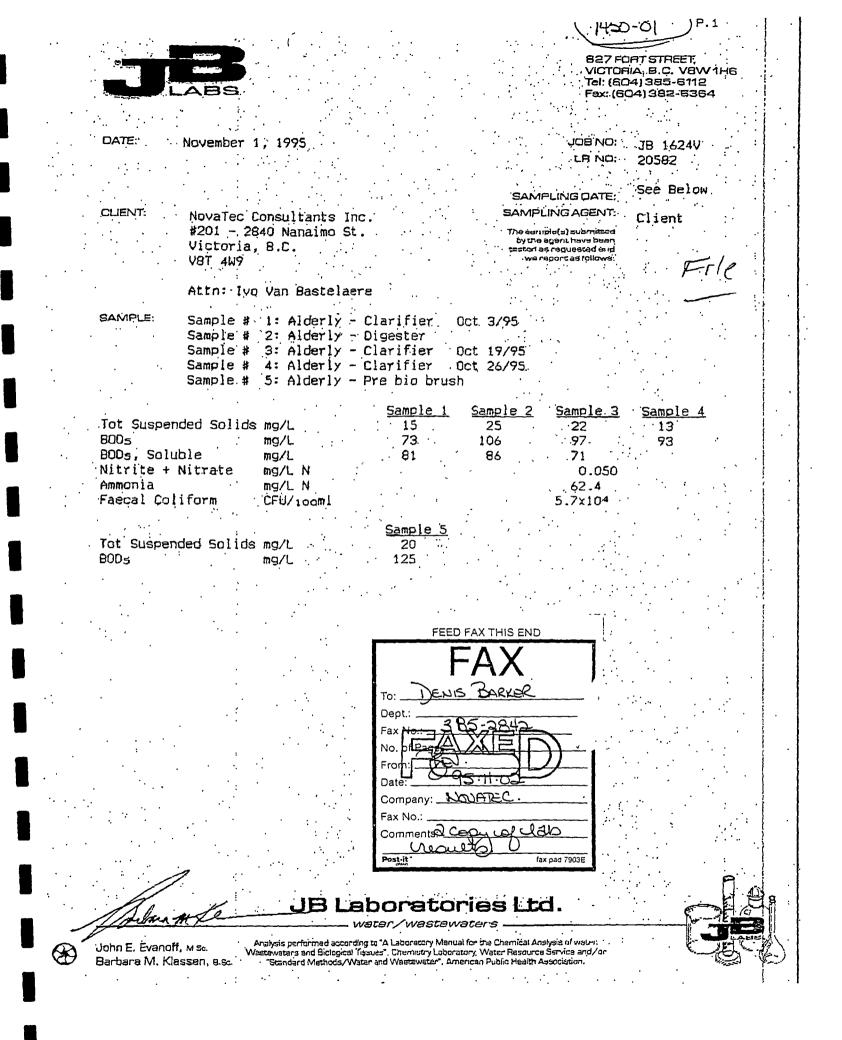


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Analysis performed according to "A Laboratory Manual for the Chemical Analysis of water, Wastewaters and Biological Tissues", Chemistry Luboratory, Water Resource Service and/or "Standard Mathoda/Water and Wastewater", American Public Health Association. . .

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		BB	•		· ·	VICTOR Tel: (60	RT STREET IA. B.C. VBW 11 4) 385-6112 04) 382-6364	LOR , J 50 НБ
-	DATE: '	November 1	, 1995 RECEIVED	NOV 2 0 199	5	JOB NO: LR NO:	JB 1624V 20582	
			RECEIVED		SAMF	LING DATE:	See Below	
	CLIENT:	NovaTec Co	onsultants Inc.		SAMPL	ING AGENT:	Client	
		#201 - 28 Victoria, V8T 4W9	40 Nanaimo St. B.C.	-	by the a tested as	ble(s) submitted agent have been a requested and aport as follows:	· . `	
		Attn: Ivo	Van Bastelaere	<b>;</b>				
	SAMPLE:	Sample # Sample #	1: Alderly - 0 2: Alderly - 0 3: Alderly - 0 4: Alderly - 0 5: Alderly - P	Digester Clarifier ( Clarifier (	Det 3/95 Det 19/95 Det 26/95			
	Tot Suspen 80D5 80D5, Solu Nitrite + Ammonia Faecal Col	Nitrate	mg/L mg/L mg/L mg/L N mg/L N CFU/100ml	<u>Sample 1</u> 15 73 81	<u>Sample 2</u> 25 106 86	Sample 3 22 97 71 0.050 62.4 5.7x10 ⁴	<u>Sample 4</u> 13 93	
	Tot Suspen BODs	ded Solids	mg/L mg/L	<u>Sample 5</u> 20 125				、 ⁻

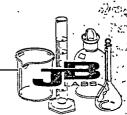
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John E. Evanoff, Misc Barbara M. Klassen, eisc JB Laboratories Ltd.

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Analysis performed according to "A Laboratory Manual for the Chemical Analysis of water, Wastewaters and Biological Tissues", Chemistry Laboratory, Water Resource Service and/or "Standard Methods/Water and Wastewater", American Public Health Association



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	'95 15:13 J	B LABORATORIES	LTD	1450-01	VICTOF Tại. (60	P.1 PRT STREE I. NA. 8 C VEVV1H6 P4)385-6112 D4)382-5364
DATE	November 2	2, 1995	,		JOB NO. - LR NO:	JB 1624V 20859
CLIENT:	#201 - 28 Victoria, V8T 4₩9	,		SAMPL The samp by the s	PLING DATE: ING AGENT - ale(s) submitted igenthave been is requested and ipport as fullows	See Below . Client
SAMPLE	Sample # Sample # Sample # Sample #	Van Bastelaen 1: Alderly - 2: Alderly - 3: Alderly - 4: Alderly - 5: Alderly -	Clarifier Clarifier Macerated In Influent	Oct 27/95 Nav 16/95 fluent Nov	• 17/95	
BODs BODs, Sol Nitrite + Ammonia	Nitrate	mg/L mg/L mg/L mg/L N mg/L N mg/L N CFU/100ml	<u>Sample 1</u> 20 99 84	<u>Sample 2</u> 32 140 105 0.004 59.6 70.4	<u>Sample 3</u> 428 540 230 0.007 34.3 142 3.1x10 ⁶	Sample 4 34 210 170 0.003 34.6 122 2.2x10 ⁴
Tot Suspe BODs	nded Solids	mg/L mg/L	34 140		FE	ED FAX THIS END
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John E. Evenoff, Mis. Barbara M. Klassen, Bise

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Analysis performed according to "A Laboratory Manual for the Chemical Analysis of water, Wastawaters and Biological Tissues", Chamistry Laboratory, Water Resource Service and/or "Standard Methods/Water and Wastawater", Amencan Public Health Association

JB Laboratories Ltd.

- water/wastewaters _

. DEC 06	'95 12:29 J	B LABORATORIES	5 LTD			P.1	1450-01
	ABS			`	VICTOF Tel· (60	DRT STREET, NA, B C V8VV D4) 385-6112 D4) 382-6364	
DATE:	December é	, 1995		- - ,	JOB ND: LR NO:	, JB 1624V 20859	pro bro
CLIENT		Consultants Ir 140 Nanaimo St B.C.		SAMPL The sem by the to=the d	PLING DATE: LING AGENT ple(s) submitted agent have been a requested and apert as follows:	See Below Client	
	Attn: Ivo	Van Bastelae	re	•			. `
SAMPLE.	Sample # Sample # Sample # Sample #	1: Alderly - 2: Alderly - 3: Alderly - 4: Alderly - 5: Alderly - 6: Alderly -	Clarifier Macerated In Influent Digester	1450-01 Nov 16/95 fluent Nov Nov 30/95	Oct 27/95		
Tot Suspen 8005 8005, Solu Nitrite + Ammonia T.Kjeldahł Faecal Col	Nitrate Nitrogen	mg/L mg/L mg/L mg/L N mg/L N mg/L N CFU/100ml	<u>Sample 1</u> 20 99 84	<u>Sample 2</u> 32 140 105 0.004 59.6 70.4	<u>Sample 3</u> 428 540 230 0.007 34.3 142 3.1x10 ⁴	<u>Sample 4</u> 34 210 170 0.003 34.6 122 2.2x10 ⁶	ı
Tot Suspen BODs BODs, Solu	ded Solids ble	mg/L mg/L mg/L	<u>Sample 5</u> 34 140	<u>Sample '&amp;</u> 46 118 142	To Dept Fax No From Date Compa Fax No Compa Fax No Compa	Pages 1 +20. 95.10 Inv vesult	
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Analysis porformed according to "A Lacoratory Manual for the Chemical Analysis of watar, Wastawaters and Biological Tissuaa" Chemistry Laboratory Water Resource Service and/or "Standard Methods/Water and Wastawatar", American Public Health Assoc ation e

JB Laboratories Ltd.

John E, Evanoff, м se Barbara M Klassen, asc

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DATE:

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827 FORT STREET. VICTORIA, 8.C. V8W1H6 Tel: (604) 385-6112 Fax: (604) 382-6364

JCB NO: JB 1624V LFI NO: 20956 Dec 4/95 SAMPLING DATE: SAMPLING AGENT: Barker

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The sample(3) sub(niifed By the agent have been tested as requested and we report as follows:

Attn: Ivo Van Bastelaere

SAMPLE: Sample # 1: Alderly - Clarifier Dec 4/95.

NovaTec Consultants Inc.

#201 - 2840 Nanaimo St.

			Sample
Tot Suspended	Solids mg/L		22
800s	mg/L		116
BODs, Soluble	mg/L	•	. 90

December 11, 1995

Victoria, B.C.

V8T 4W9

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Dept.		
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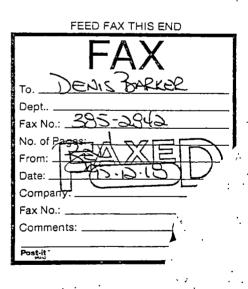
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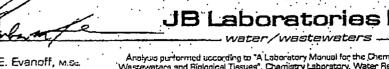
John E. Evanoff, M.Sa. Barbara M. Klassen, a.sa.

Analysis purformed according to "A Lubor atory Manual for the Chemical Analysis of water, "" Wastewaters and Biologoui Tissues", Chemistry Laboratory, Water Resource Service and/or "Standard Methods/Water and Wastewater", American Public Health Association.

DEC 18 '95 14:41 JB LABORATORIES LTD

DATE: December 18, 1995 JOBINO: JB 1624V LA NO: 20956 SAMPLINGCOATE: See Below CLIENT: NovaTec Consultants Inc. SAMPLINGACENT: #201 - 2840 Nanaimo St. The sumpleted submitted Victoria, B.C. VBT 4W9 Attn: Ivo Van Bastelaere SAMPLE: Sample # 1: Alderly - Clarifier Dec 4/95 Sample # 2: Alderly - Clarifier, Dec 13/95 Tot Suspended Solids mg/L Sample 1 BODs mg/L 116 131 BODs, Soluble mg/L 90			827 FORT STREET. VICTORIA, B.C. V8VV 1HE Tel: (604) 385-6112 Fax: (604) 382-8364
CLIENT: NovaTec Consultants Inc. #201 - 2840 Nanaimo St. Victoria, B.C. Victoria, B.C. Attn: Ivo Van Bastelaere SAMPLE: Sample # 1: Alderly - Clarifier Dec 4/95 Sample # 2: Alderly - Clarifier, postair Dec 13/95 Tot Suspended Solids mg/L BODs mg/L Sample 1 Sample 2 116 131	•	DATE:	December 18, 1995 JOB NO: JB 1624V
CLIENT: NovaTec Consultants Inc. #201 - 2840 Nanaimo St. Victoria, B.C. V8T 4W9 Attn: Ivo Van Bastelaere SAMPLE: Sample # 1: Alderly - Clarifier Dec 4/95 Sample # 2: Alderly - Clarifier, postair Dec 13/95 Tot Suspended Solids mg/L BODs mg/L 16 131			
#201 - 2840 Nanaimo St.   The sample(s) submitted   Client     #201 - 2840 Nanaimo St.   The sample(s) submitted   The sample(s) submitted     Victoria, B.C,   The sample(s) submitted   The sample(s) submitted     VBT 4W9   Natth: Ivo Van Bastelaere   The sample(s) submitted     SAMPLE:   Sample # 1: Alderly - Clarifier   Dec 4/95     Sample # 2: Alderly - Clarifier, postair   Dec 13/95     Tot Suspended Solids mg/L   22   18     BODs   mg/L   116   131	•		SAMPLING DATE: See Below
SAMPLE: Sample # 1: Alderly - Clarifier Dec 4/95 Sample # 2: Alderly - Clarifier, postair Dec 13/95 Tot Suspended Solids mg/L <u>Sample 1</u> BOD ₅ mg/L 116 131	·	CLIENT:	#201 - 2840 Nanaimo St. Victoria, B.C.
Sample # 2: Alderly - Clarifier, postair Dec 13/95      Sample # 2: Alderly - Clarifier, postair Dec 13/95     Sample 1   Sample 2     Tot Suspended Solids mg/L   22   18     BODs   mg/L   116   131			Attn: Ivo Van Bastelaere
Tot Suspended Solids mg/L 22 18 BODs mg/L 116 131		SAMPLE:	Sample # 1: Alderly - Clarifier Dec 4/95 Sample # 2: Alderly - Clarifier, postair Dec 13/95
		800s	ded Solids mg/L 22 18 mg/L 116 131





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John E. Evanoff, M.S.. Barbara M. Klassen, 9.S.

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Analysis performed according to "A Laboratory Manual for the Chemical Analysis of water. Waszewatara and Biological Tissues", Chamistry Laboratory, Water Resource Service and/or "Stundard Method:/Water and Wastewater", American Public Health Association.

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	DATE:	January 10, 1996		JOB NO;	
		January 10, 1776		LR NO:	JB 1624V 20956
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				SAMPLING DATE:	See Below
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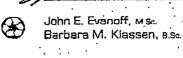
· · · · ·	#201 - 2840 Nanaimo S Victoria, B.C.			The earnple(s) submitted by the agent have been tested as requested and
	V8T 4W9		· · · · ·	wareportasiollows:
	Atto: Ivo Van Bastela	ere	· · · ·	가지 같은 가슴이 있다. 이 가 가 나는 것이 있는 것이 있다.

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SAMPLE:	Sample	# ·1:	Alderly - Clarifier	Dec 4/95
	 Sample	# 2:	Alderly - Clarifier.	Dec 13795
	Sample	∦ 3;	Alderly - Clarifier	Dec 21/95
•		•		•

Tot Suspende	≥d Solids mg/L	. · .	Sample 1	Sample 2	Sample 3
8005	mg/L	• •	116	131	110
BODs, Solubl	le mg/L		<b>9</b> 0		



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Analysis performed according to "A'Laboratory Manual for the Chemical Analysis of wath, Watuwaters and Biological Tissues", Chemistry Laboratory, Water Resource Survice and/or "Standard Methods/Water and Wastewater", American Public Health Association. ...

JB Laboratories Ltd. - water/wastewaters

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