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**RADIATION EFFECTS ON  
p- AND n- TYPE CATALYSTS USED  
IN THE THERMAL DISSOCIATION  
OF ETHYL ALCOHOL**

**MATTEO DONATO**

**MINERAL SCIENCES DIVISION**

**DEPARTMENT OF MINES AND  
TECHNICAL SURVEYS, OTTAWA**

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RADIATION EFFECTS ON p- AND n-TYPE CATALYSTS  
USED IN THE THERMAL DISSOCIATION OF ETHYL ALCOHOL

by

Matteo Donato<sup>\*</sup>

- - -

SYNOPSIS

The dissociation of anhydrous ethyl alcohol has been studied over the temperature range 330°-430°C with the employment of catalysts that had been exposed to a range of estimated "integrated" neutron doses of up to  $96.6 \times 10^{18}$  n/cm<sup>2</sup>. The catalysts are ZnO, an n-type semiconductor, prepared by decomposition of the carbonate, and Cr<sub>2</sub>O<sub>3</sub>, a p-type semiconductor, prepared by dehydration of the hydroxide. Measurable changes in yield and decomposition mechanism have been observed as compared with the unirradiated catalysts.

The variation in the behaviour of the catalysts has been related to the various neutron doses received, and the results are discussed in the framework of the electronic theory of catalysis on semiconductors.

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\* National Research Council Postdoctorate Fellow, Physics and Radiotracer Subdivision, Mineral Sciences Division, Mines Branch, Department of Mines and Technical Surveys, Ottawa, Canada.

Direction des mines

Rapport de recherches R.105

EFFETS DE LA RADIATION SUR LES CATALYSEURS  
DE TYPE "p" ET "n" QUI SERVENT À LA DISSOCIATION  
THERMIQUE DE L'ALCOOL ÉTHYLIQUE

par

Matteo Donato\*

RÉSUMÉ

La dissociation d'alcool éthylique anhydre a été étudiée dans la zone de température 330° - 430°C à l'aide de catalyseurs qui avaient été exposés à une série de dosages "intégrés" de neutrons qui pouvaient atteindre jusqu'à  $96.6 \times 10^{18} \text{ n/cm}^2$ . Les catalyseurs en cause sont le ZnO, semi-conducteur de type "n" obtenu par décomposition du carbonate, et le Cr<sub>2</sub>O<sub>3</sub>, semi-conducteur de type "p" obtenu par déshydratation de l'hydroxyde. L'auteur a noté des changements mesurables dans le rendement et le mécanisme de décomposition au regard de l'emploi de catalyseurs non irradiés.

La variation dans le comportement des catalyseurs a été attribuée aux diverses doses de neutrons reçues, et l'auteur traite des résultats dans le cadre de l'hypothèse électronique de catalyse relativement aux semi-conducteurs.

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\*Boursier du Conseil national de recherches, Subdivision de la physique et des indicateurs radio-actifs, Division des sciences minérales, Direction des mines, ministère des Mines et des Relevés techniques, Ottawa, Canada.

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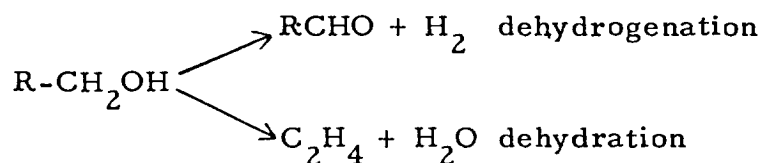
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## INTRODUCTION

In recent years, there has been an increasing interest in the effect of nuclear radiation on solid inorganic catalysts. This is due to the fact that catalytic behaviour is strongly dependent on the structure and energy conditions of the catalyst and its structure may be modified under nuclear irradiation (1, 2, 3, 4). The object of the present report is to discuss the behaviour, as catalysts, of ZnO, an n-type semiconductor, and Cr<sub>2</sub>O<sub>3</sub>, a p-type semiconductor, before and after irradiation in the Chalk River reactor. Studies have been made of the well-known thermal dissociation reaction of ethyl alcohol that proceeds along two paths:



The particular reaction path taken is determined at the first stage of reaction, the adsorption of the alcohol molecule, and depends on the particular bond broken in the molecule, the OH or C-OH bond; this in turn depends on the nature of the catalyst. With ZnO and Cr<sub>2</sub>O<sub>3</sub> catalysts both reactions occur.

It is well known that the reactor irradiation of a solid semiconductor can generally produce the following effects: a) direct ionization; b) change in the degree of disorder in the lattice of the solid irradiated; and c) nuclear reaction in the solid. Each of these effects produces a variation in the number of free carriers in the solid. The first effect is only a temporary effect. The second one can be removed by heating the sample at a high temperature. The third one, which leads to the production of impurities of different chemical character in the lattice of the solid, is a permanent effect and irreversible.

In the past twenty years many authors, such as Hauffe (5), Schwab (6), Garner (7), Wolkenstein (8) and others, have developed an electronic theory of catalysis on semiconductors. According to this theory the nature of the substrate bonding determines the transfer of electrons from the adsorbed molecule to the unfilled electronic levels in the solid catalyst, or from the solid catalyst with an excess of electrons to the adsorbed molecule. This picture of catalysis on semiconductors has been supported by the publications of many research workers. The well-known catalytic activity of the transition metals is thus correlated with their unfilled d-bands, and the different activities of n- and p-type semiconductors with their capability to donate or accept electrons.

In this framework, the gamma and neutron irradiation of a solid catalyst would be expected to alter its catalytic activity, because the products of irradiation include trapped electrons and holes (in non-metals), displaced atoms, and impurities of a different chemical nature, due to the neutron-induced transmutations, all of which influence the electronic structure of the solid catalyst and hence its ability to interchange electrons with the adsorbed molecules on the surface.

It has been reported by Wolkenstein (8) that the relative activity of the catalyst—in this case, for dehydration or dehydrogenation—depends on the position of the Fermi level and that the lowering of this level retards dehydrogenation and accelerates dehydration. Some factors that affect the position of the Fermi level include: acceptor impurities, donor impurities, nuclear radiation.

#### APPARATUS AND PROCEDURE

The reaction, the decomposition of the ethyl alcohol, was observed at atmospheric pressure and at temperatures within the range 330°-390°C for ZnO and 370°-430°C for Cr<sub>2</sub>O<sub>3</sub>. The experiments were carried out in a continuous flow reactor made of quartz glass.



The apparatus used in the present study consisted of an alcohol feeding system, a vaporizing unit, a reactor, an ethanol recovery system and a gas-measuring device. (Figure 1 shows a schematic diagram of the apparatus.) The entire apparatus was made of quartz glass except for the condenser and the receiver. A Milton-Roy "Minipump", made of stainless steel, was used for the ethanol feed system to ensure a constant slow rate of gas flow. A water condenser (0°C) and a dry-ice acetone trap (-40°C) in series were used to condense the liquid products. The volume of the gaseous products was measured with a gas volumeter. The composition of the gas mixture was determined by means of a temperature-controlled chromatographic system. The samples of gas were introduced by means of a gas-sampling valve, which provided a convenient and highly reproducible system for sampling gas streams. A portion of the gas stream to be analysed was allowed to flow continually through the valve. The temperature of the catalyst bed during the reaction was measured and recorded by a chromel-alumel thermocouple placed in the reactor thermocouple well. Control of the reactor temperature was maintained by adjusting the voltage to the reactor heating coil.

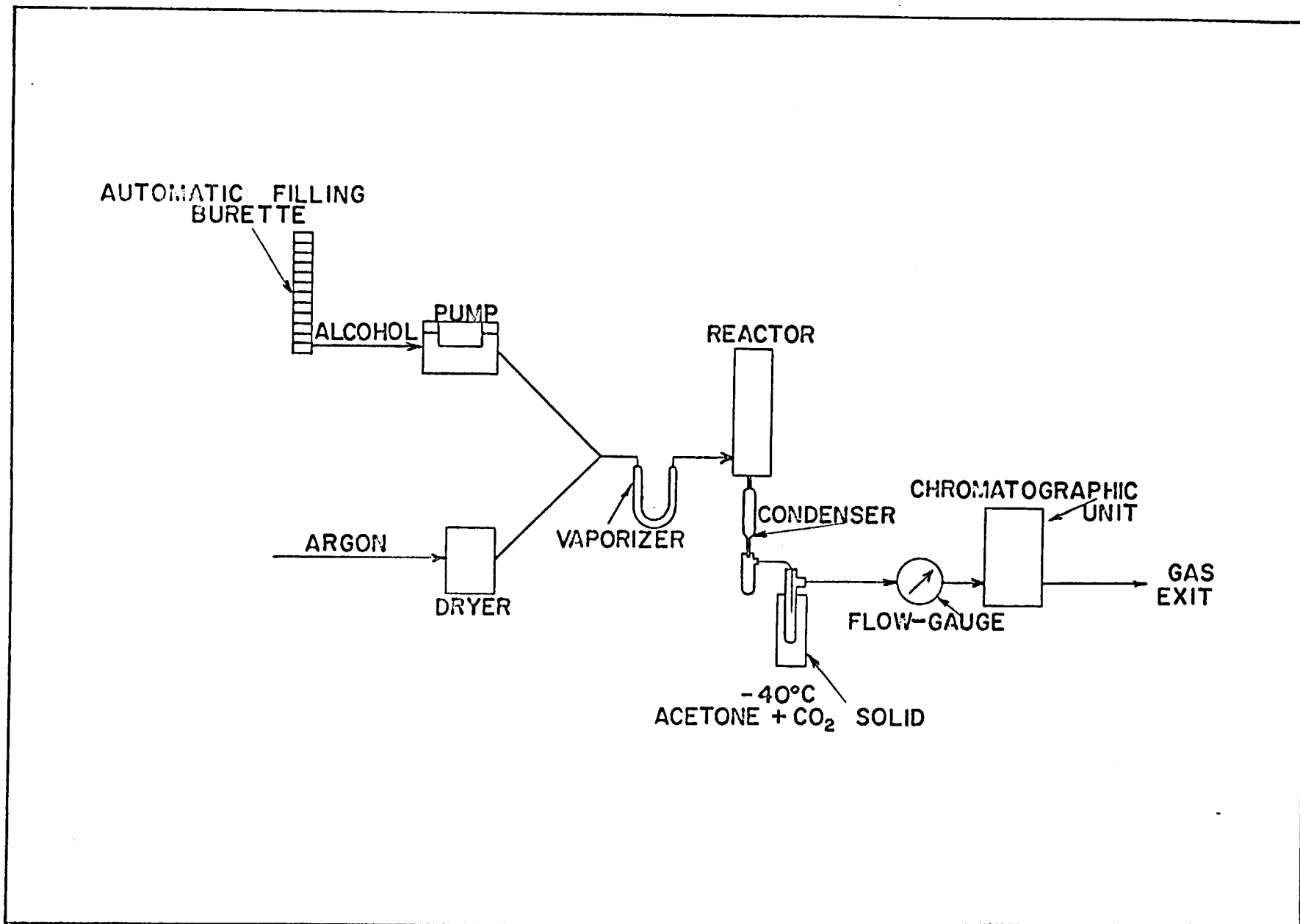


FIGURE I SCHEMATIC DIAGRAM OF APPARATUS.

## PREPARATION OF CATALYSTS

The zinc oxide catalysts were prepared by ignition of  $\text{ZnCO}_3$  at  $450^\circ\text{C}$  in air for 3 hours. The resulting powder was pressed into pellets and the latter were then crushed in order to have granules in the size range of 20-28 mesh. The amount of catalyst used in each test was 0.4 g. The surface area was  $23.7 \text{ m}^2/\text{g}$ .

The chromic oxide catalysts were prepared by precipitation of the hydroxide from a solution of the nitrate, using ammonium hydroxide as the precipitating agent. The reagents used were highly pure Mallinckrodt "Transistar" products. The precipitate was then washed, filtered, and dried. The dry hydroxide was then ground and heated at  $450^\circ\text{C}$  for 3 hours in air. The dry  $\text{Cr}_2\text{O}_3$  was pressed into pellets that were then granulated and screened to yield a 20-28 mesh product. The amount of  $\text{Cr}_2\text{O}_3$  used in each test was 0.2 g. The surface area was  $19.8 \text{ m}^2/\text{g}$ .

The alcohol feed for both series of catalyst tests was 0.204 ml/min.

Properties of the alcohol used are: refractive index  $n_D^{25} = 1.3600$ , specific gravity  $G_{20}^{20} = 0.7955$ ,  $G_4^{20} = 0.7914$ , water = 0.10% v/v, b.p. =  $78.2^\circ\text{C}$ .

Four samples of  $\text{ZnO}$  and two samples of  $\text{Cr}_2\text{O}_3$  were irradiated in the Chalk River reactor at various estimated integrated neutron doses up to  $10^{20} \text{ n/cm}^2$  at a maximum flux of  $5.8 \times 10^{13} \text{ n/cm}^2 \text{ sec}$ . The estimated gamma flux was  $1 \times 10^8$  roentgens per hour.

The spectrographic analyses for the ZnO and Cr<sub>2</sub>O<sub>3</sub> catalysts are presented in Table 1.

TABLE 1  
Analysis of Catalysts

Catalyst	Surface Area	Elements, per cent									
		Si	Mg	Fe	Cu	Ca	Al	Mn	Pb	Cd	B
ZnO	23.7 m <sup>2</sup> /g	0.02	0.005	0.004	0.002	n.d.	n.d.	n.d.	n.d.	0.08	n.d.
Cr <sub>2</sub> O <sub>3</sub>	19.8 m <sup>2</sup> /g	0.07	0.009	0.01	0.01	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.

n.d. = not detected

The reactor irradiation conditions are presented in Table 2.

TABLE 2  
a) Maximum Flux and b) Integrated Neutron Doses

Catalyst	Weight (g)	I	II	III	IV	V
ZnO	0.4	a) Not irradiated	2.3 x 10 <sup>13</sup>	3.9 x 10 <sup>13</sup>	4.6 x 10 <sup>13</sup>	4.8 x 10 <sup>13</sup>
		b) Not irradiated	13.9 x 10 <sup>18</sup>	23.3 x 10 <sup>18</sup>	59.6 x 10 <sup>18</sup>	96.6 x 10 <sup>18</sup>
Cr <sub>2</sub> O <sub>3</sub>	0.2	a) Not irradiated	3.3 x 10 <sup>13</sup>	5.8 x 10 <sup>13</sup>		
		b) Not irradiated	20 x 10 <sup>18</sup>	34.8 x 10 <sup>18</sup>		

a) Fluxes in neutrons/cm<sup>2</sup> sec

b) Neutron doses in neutrons/cm<sup>2</sup>

The experimental variables determined consisted of feed rate, reaction time, temperature, and amount of gas evolved (hydrogen and ethylene).

From these results, the behaviour of the catalyst, the reaction rates and the percentage of conversion at various temperatures were calculated and curves of percentage conversion versus temperature were plotted. Before and after each series of runs the reactor was flushed with dried argon to ensure that no air or moisture was present.

### EXPERIMENTAL RESULTS

After irradiation the zinc oxide catalysts presented a yellow-brown colour; the green chromia catalysts, on the other hand, did not show any change in colour.

In the case of  $ZnO$ , the initial experiments indicated that on a fresh catalyst surface the activity of the irradiated catalyst was lower than on the non-irradiated one, but when the catalyst was aged by use at  $390^{\circ}C$  for a few days the radioactive catalysts were more active and the ratio  $H_2/C_2H_4$ , which was changing during the first runs, reached a constant value. Figure 2 shows the reaction rate at a temperature of  $390^{\circ}C$  for normal and irradiated, stabilized

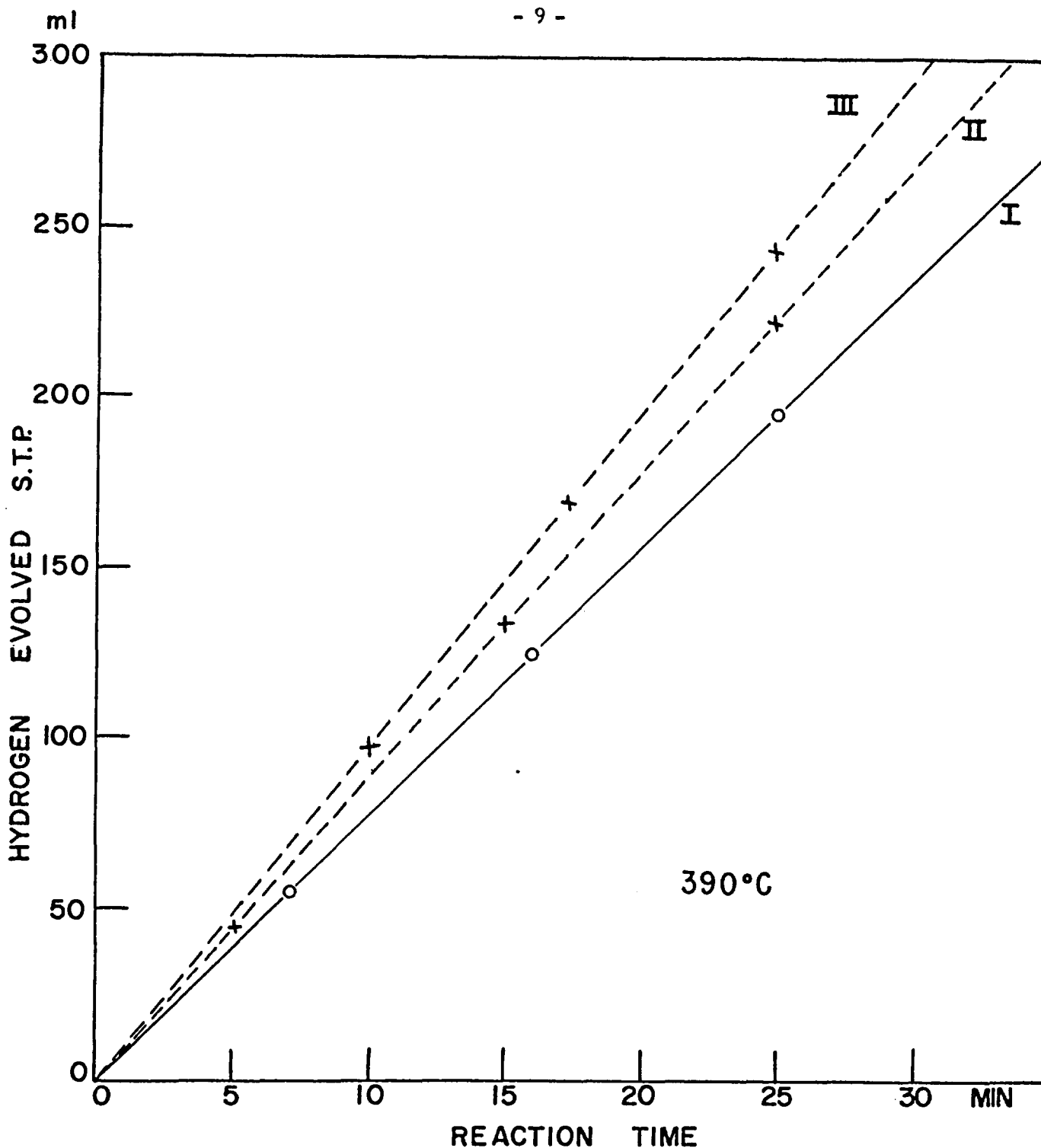


FIGURE 2 REACTION RATES FOR DIFFERENT CATALYSTS - ZnO

ETHYL ALCOHOL FEED - 0.204 ml/min

NORMAL CATALYST ———○———

IRRADIATED II INTEGRATED NEUTRON DOSE ---+---  $13.9 \times 10^{18} \text{ n/cm}^2$

III INTEGRATED NEUTRON DOSE ---+---  $23.3 \times 10^{18} \text{ n/cm}^2$

catalysts. Figure 3 compares the proportion of hydrogen and ethylene evolved for normal and irradiated catalysts. Figures 4, 5 and 6 report the per cent conversion to hydrogen and ethylene, and the total conversion versus the integrated neutron doses that the catalysts received over the range of temperatures studied. It is evident that the nuclear irradiation significantly affects the reaction paths (see Figure 3) and the effect increases with irradiation times or estimated integrated neutron doses of the solid catalyst, to reach an asymptotic value of the ratio  $H_2/C_2H_4$ , as can be seen in Figure 7.

According to Wolkenstein (8) and Garner (10), the dehydrogenation of ethyl alcohol is an acceptor or n-type reaction; in other words, this is a reaction accelerated by the presence of free electrons and it proceeds more rapidly the higher is the Fermi level (other conditions being equal). In contrast, the dehydration is a donor or p-type reaction. In the case of ZnO it is evident that a higher Fermi level has been obtained in the irradiated catalysts compared with the non-irradiated one and this leads to an increase in the hydrogen/ethylene ratio in the reaction products. There is also an increase in the dehydrogenation activity of the same catalysts, which seems to be a function of the estimated integrated neutron dose of the catalysts (see Figures 2-4) or of the amount of gallium-69 created. The dotted line in Figure 4 indicates the shift with temperature in the neutron dose required for maximum hydrogen conversion.

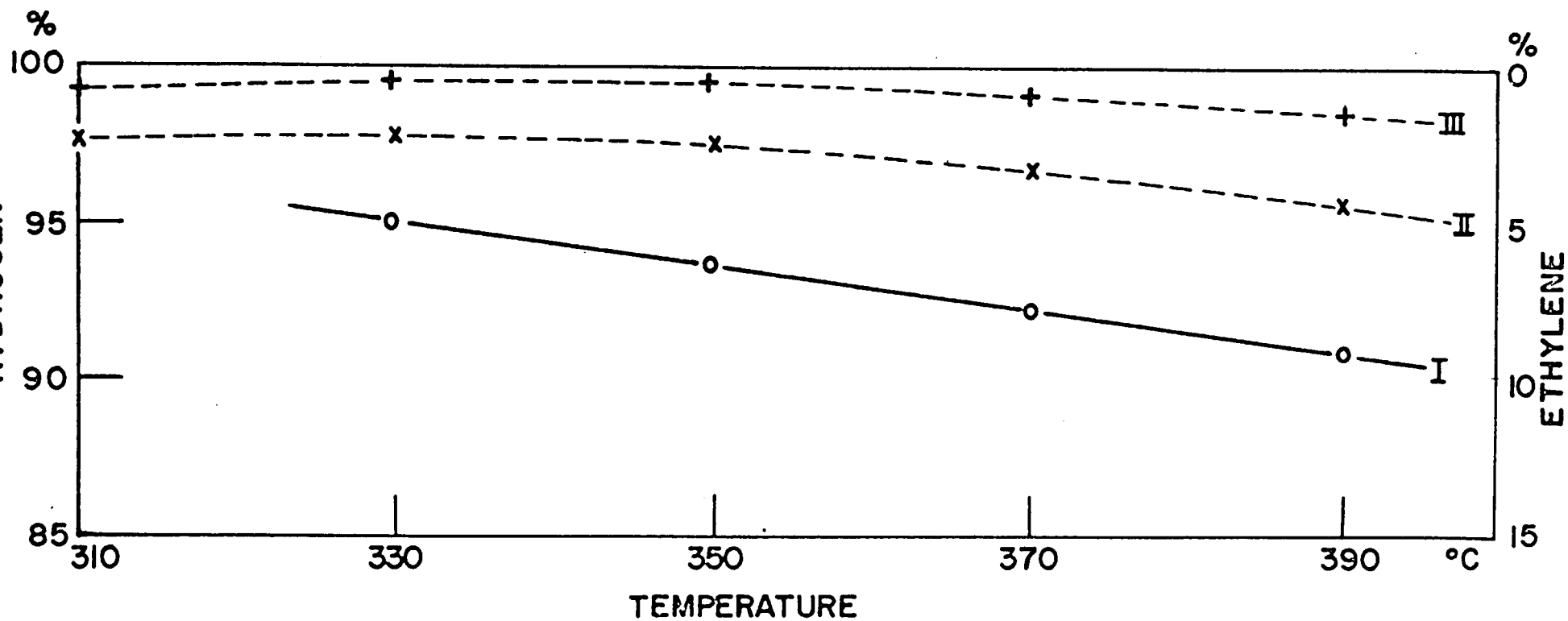


FIGURE 3 BEHAVIOUR OF ZINC OXIDE CATALYSTS AT VARIOUS TEMPERATURES

ETHYL ALCOHOL FEED = 0.204 ml/min

CATALYST- ZnO TYPE A, 0.4g, 20-28 MESH

NORMAL CATALYST: ———○———

IRRADIATED II      - - - - x - - - - INTEGRATED NEUTRON DOSE       $13.9 \times 10^{10} \text{ n/cm}^2$

                         III      - - - - + - - - - INTEGRATED NEUTRON DOSE       $23.3 \times 10^{10} \text{ n/cm}^2$



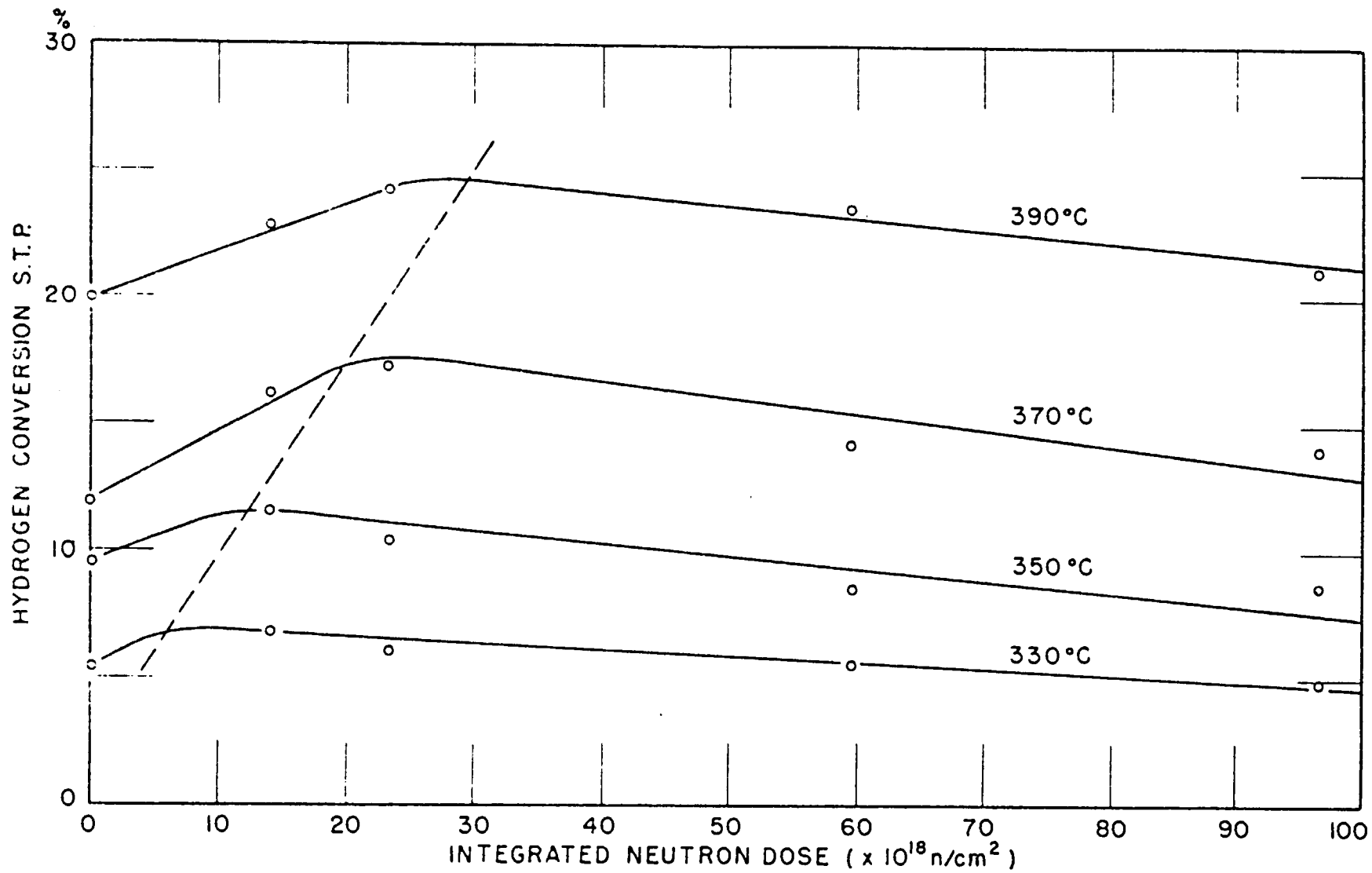


FIGURE 4 ZnO CATALYST-EFFECT OF NEUTRON DOSES ON HYDROGEN YIELD

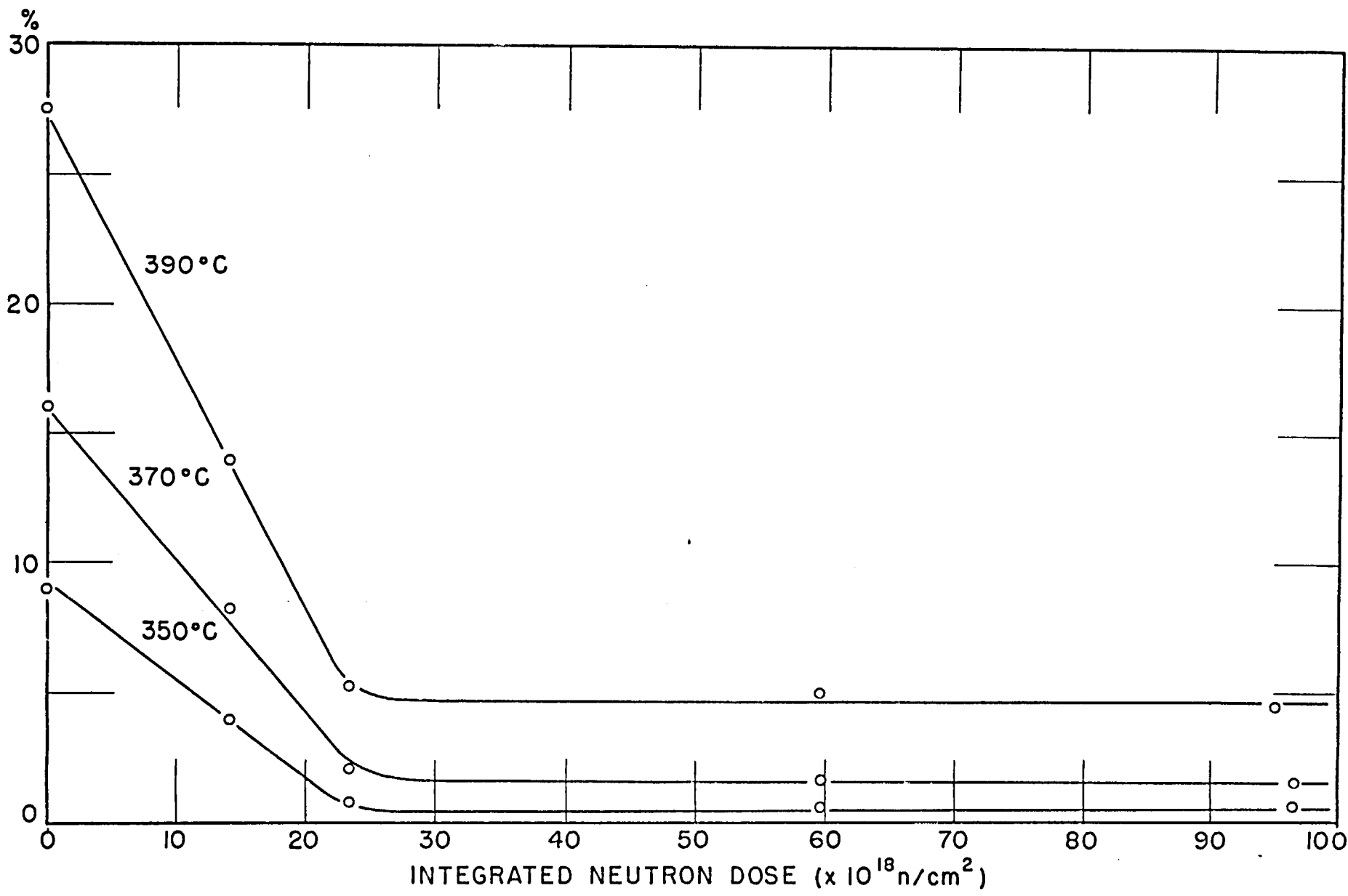


FIGURE 5 ZnO CATALYST- EFFECT OF NEUTRON DOSES ON ETHYLENE YIELD.

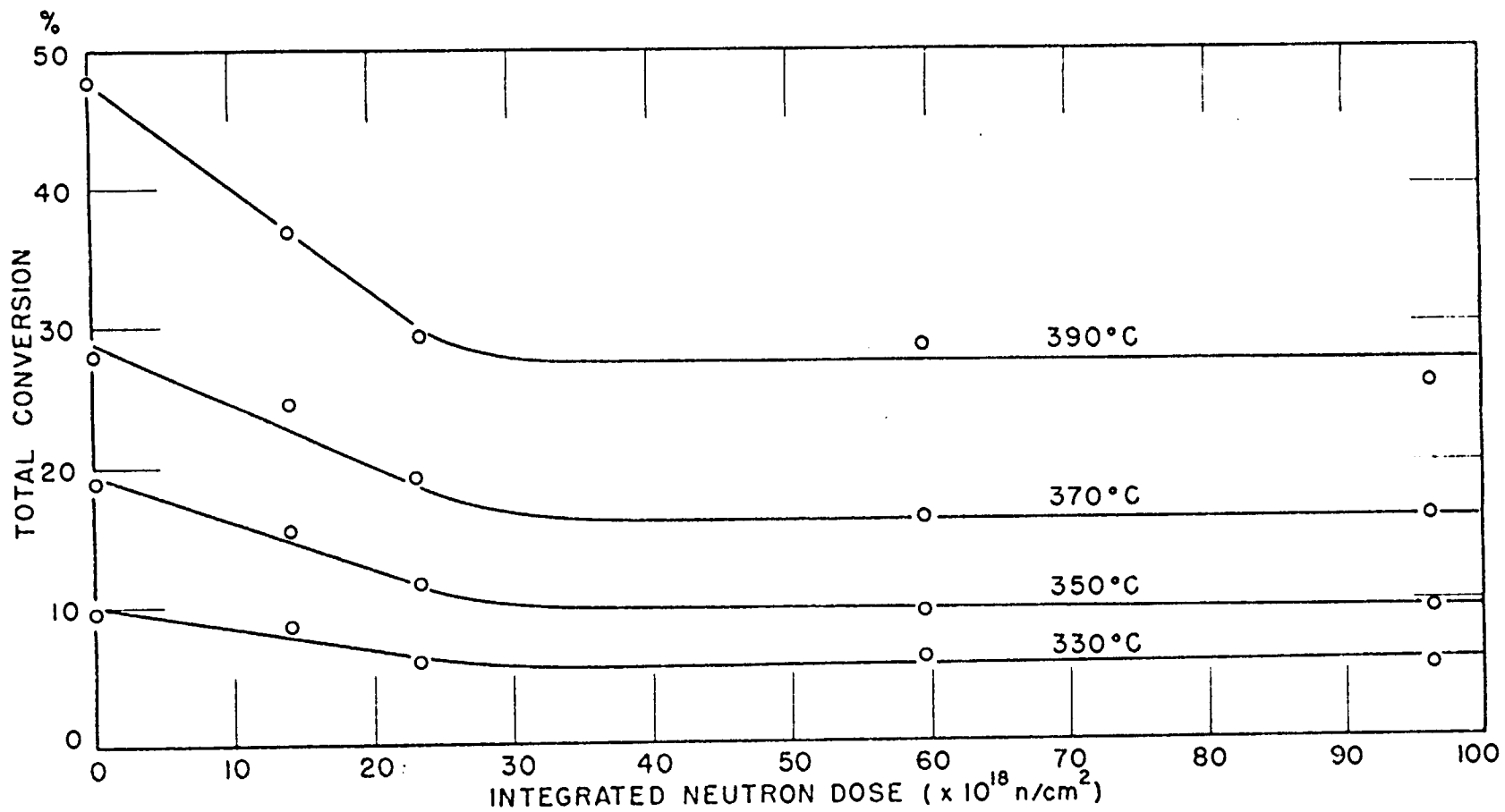


FIGURE 6 ZnO CATALYST - EFFECT OF NEUTRON DOSES ON TOTAL CONVERSION

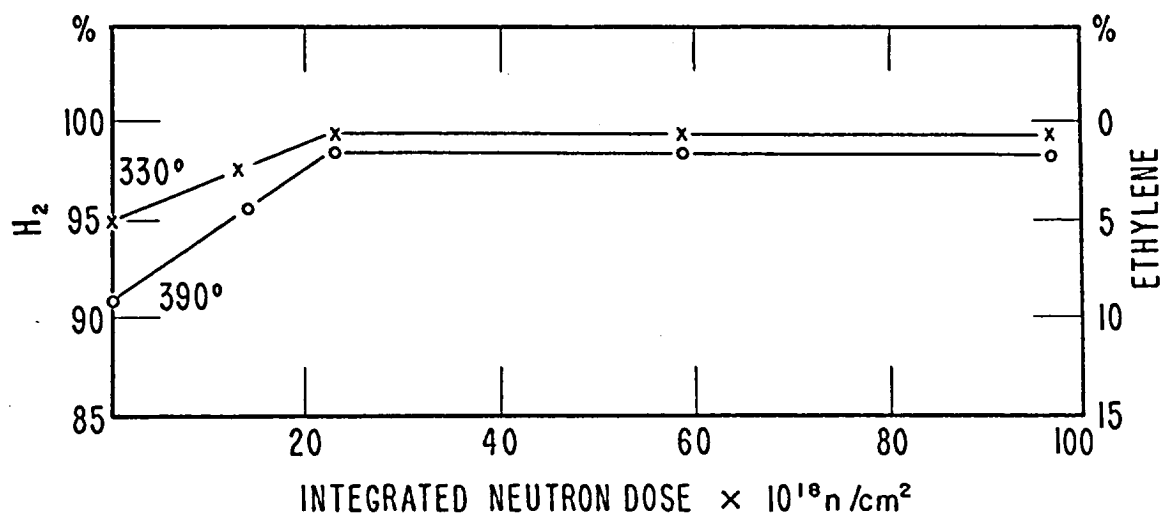


FIGURE 7 BEHAVIOUR OF ZnO AT VARIOUS INTEGRATED NEUTRON DOSES.

The neutron irradiation of ZnO results in nuclear transmutations in the solid, which lead to the production of impurities (mainly gallium-69) of different chemical character in the specimen, and obviously this is an irreversible process.

The natural abundance of Zn-68 is 18.57% in the zinc element, its neutron cross-section is 1.06 barn, and the half-life of Zn-69 is 52 min (11). Because of this short half-life, creation of gallium is practically complete by the time of receipt of the irradiated sample. An approximate calculation of the amount of gallium-69 created by nuclear transmutation of Zn-68 in the catalyst samples used is reported in Table 3.

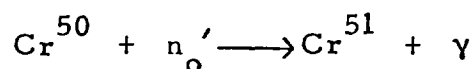
TABLE 3  
Production of Ga-69 in Irradiated ZnO

Catalyst: ZnO	Integrated Neutron Dose	Ga-69 (ppm)
I	0	0
II	$13.9 \times 10^{18} \text{ n/cm}^2$	2.64
III	$23.3 \times 10^{18} \text{ n/cm}^2$	4.84
IV	$59.6 \times 10^{18} \text{ n/cm}^2$	12.2
V	$96.6 \times 10^{18} \text{ n/cm}^2$	22.0

Gallium is a donor impurity in ZnO.

For the first four catalysts, the amount of copper-65 produced by transmutation of the isotope zinc-64 is of the order of 0.2-1 ppm, about 1/20 of the amount of copper initially present as an impurity in the non-irradiated catalyst, and becomes quite appreciable (2 ppm) at the largest neutron doses and after a long period of decay (Catalyst V). Copper is an acceptor impurity if present in the form of  $\text{Cu}^{++}$ ; in fact it lacks an electron in its closed shell. It may act as donor if present as Cu atom, that is, characterised by one electron in excess in the closed shell, while the  $\text{Cu}^+$  ion possesses a closed electron shell (8).

The exposure to neutron and gamma irradiation of the  $\text{Cr}_2\text{O}_3$  catalysts did not show any shifting in the reaction path of the catalyst (Figures 8-11) and resulted in a decrease in the activity of the two chromic oxide catalysts, as seen in Figures 9 and 10. Such behaviour of the chromic oxide catalysts was expected. The neutron irradiation of  $\text{Cr}_2\text{O}_3$  does not result in any nuclear transmutation such as to create significant impurities of different chemical character in the specimen, and the only transmutation created is:



Chromium-51 decays by K-capture with a 27.8-day half-life to vanadium-51, which is stable. The tests described here were done before there was any appreciable decay of chromium-51.

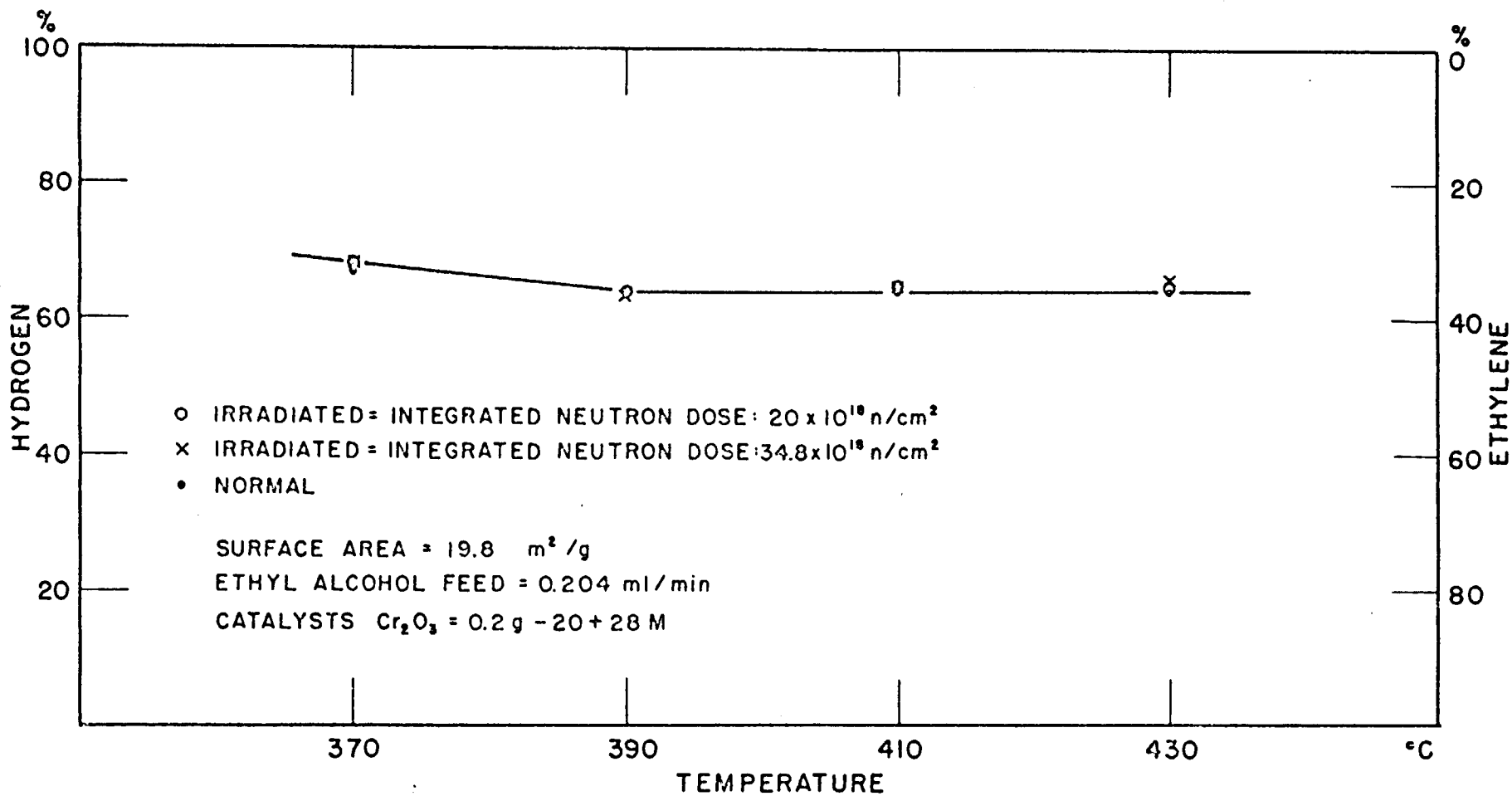


FIGURE 8 BEHAVIOUR OF Cr<sub>2</sub>O<sub>3</sub> CATALYSTS AT VARIOUS TEMPERATURES

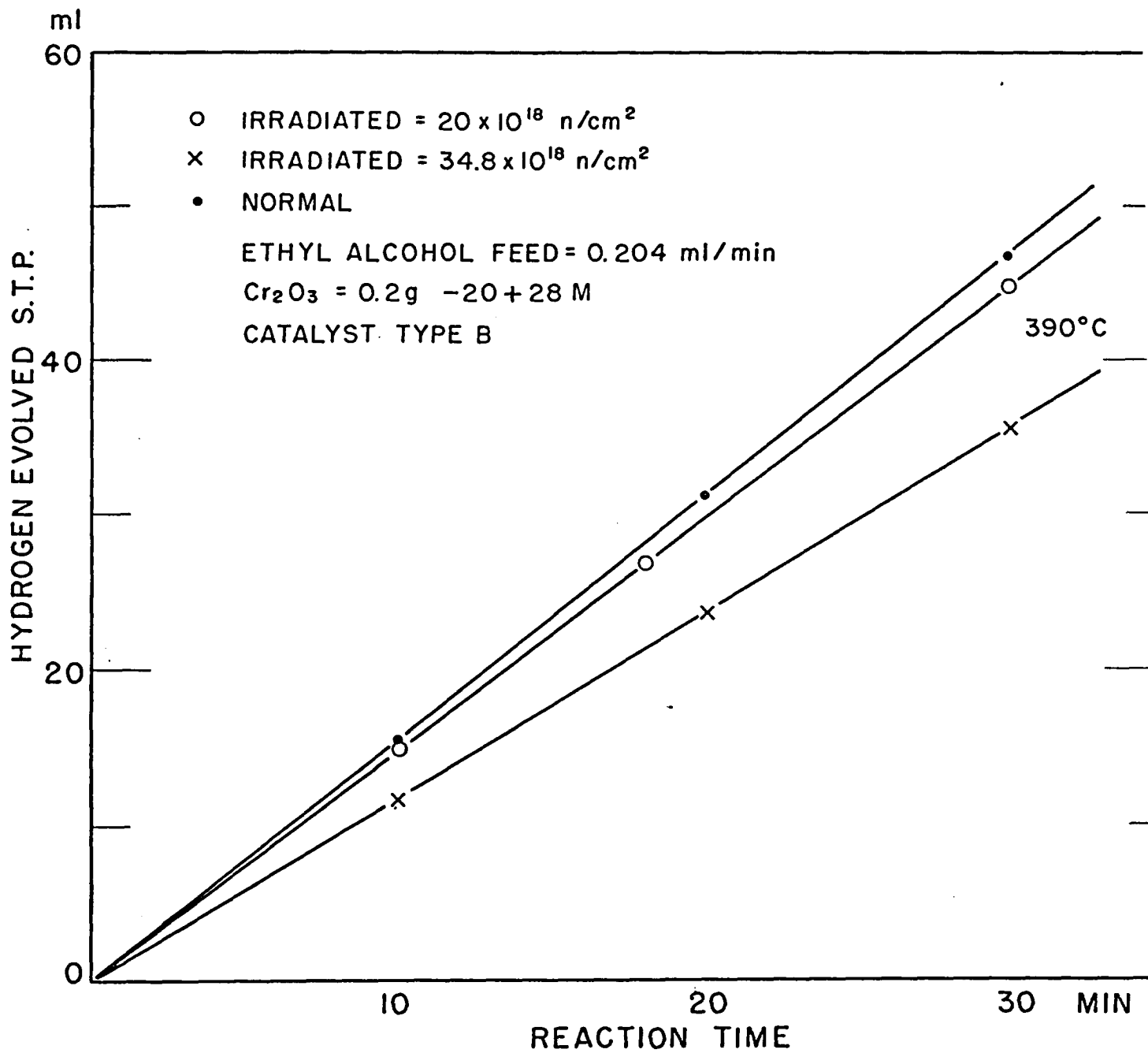


FIGURE 9 REACTION RATES FOR Cr<sub>2</sub>O<sub>3</sub> CATALYSTS.



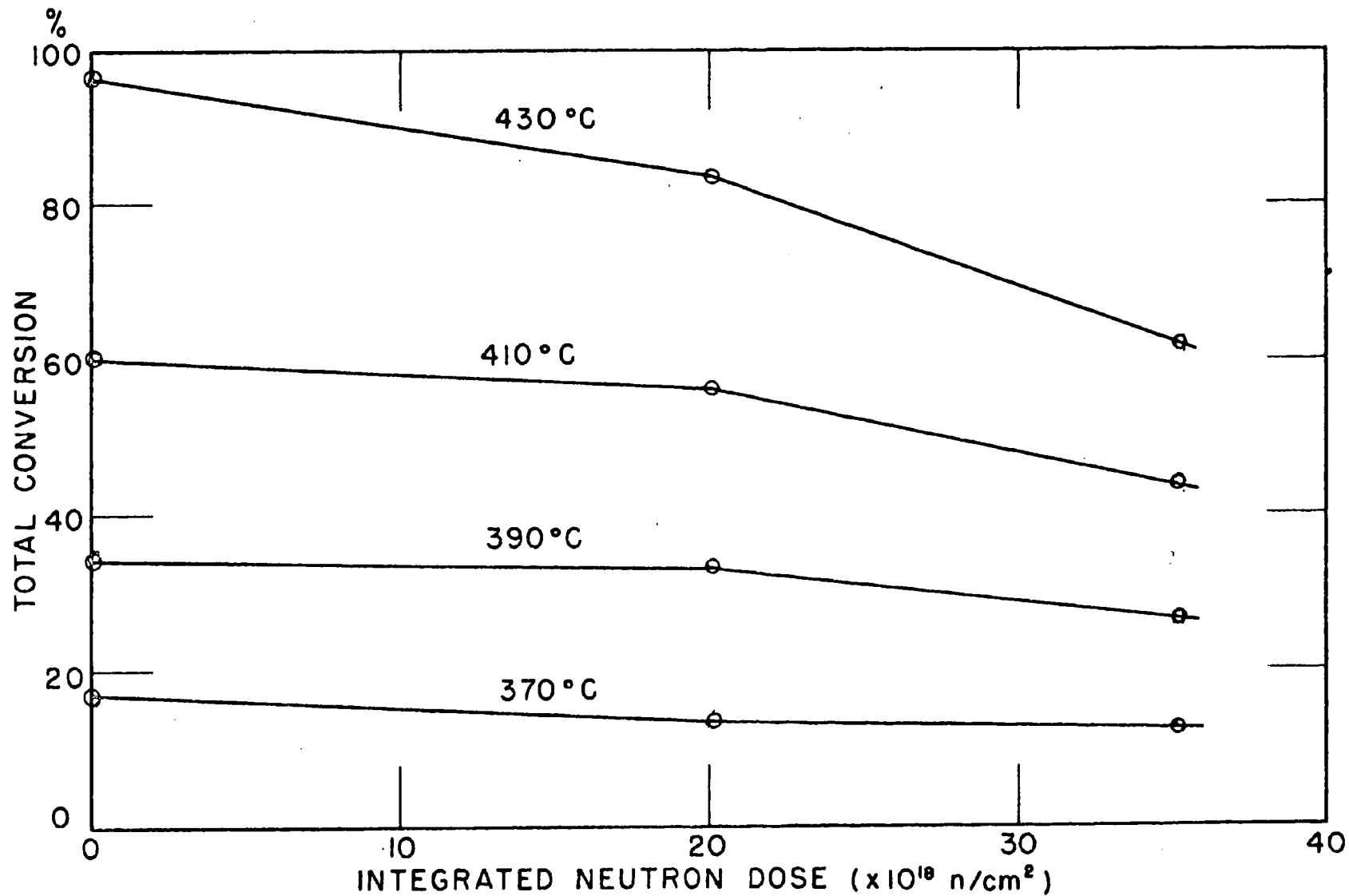


FIGURE 10 TOTAL CONVERSION AT VARIOUS INTEGRATED NEUTRON DOSES --  
 $\text{Cr}_2\text{O}_3$  CATALYST

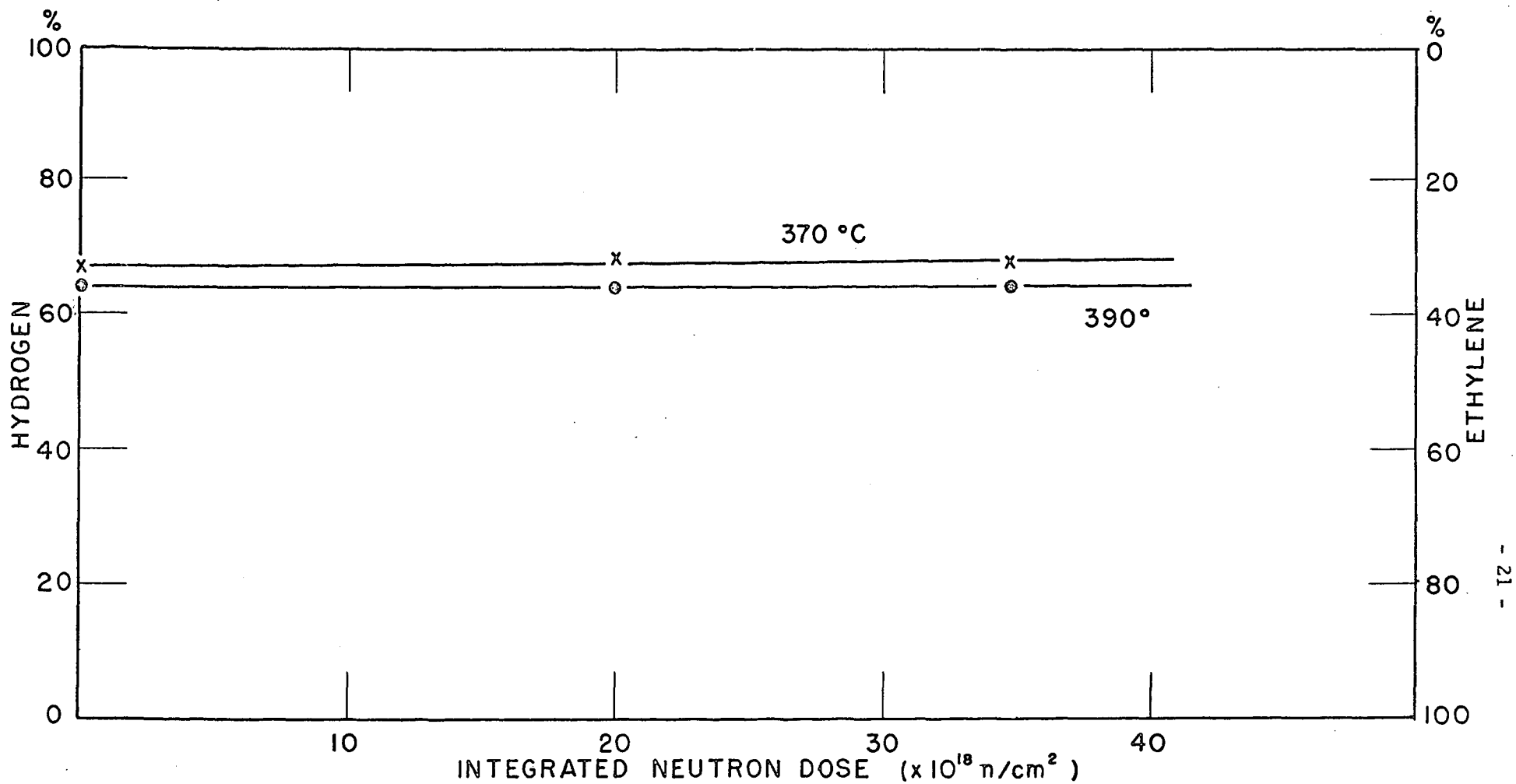
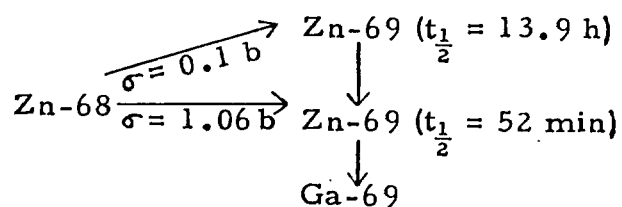


FIGURE II BEHAVIOUR OF  $\text{Cr}_2\text{O}_3$  CATALYSTS AT VARIOUS INTEGRATED NEUTRON DOSES

### CONCLUSIONS

For an n-type semiconductor it has been found by Wagner (12), Hauffe (13), Schwab (14) and others, that the charge carrier concentration can be raised by incorporating small amounts ( $\sim 0.01\%$ ) of impurities. Addition of oxides of trivalent metals, e.g.,  $\text{Al}_2\text{O}_3$  or  $\text{Ga}_2\text{O}_3$ , causes an increase, whereas oxides of monovalent metals cause a decrease, in the concentration of charge carriers. In irradiated zinc oxide both zinc and oxygen vacancies, as well as interstitial zinc atoms, are produced. Interstitial oxygen atoms are unlikely in stabilized ZnO and the displaced oxygen atoms probably go to vacancies or grain boundaries, to be freed later. The nuclear reaction



appears to be responsible for the amount of gallium present. In the range of temperatures investigated so far, it is believed that the lattice defects introduced by gamma-ray and neutron irradiation are removed slowly, and this could explain the ageing period during which the catalysts present a lower activity and a lower  $\text{H}_2/\text{C}_2\text{H}_4$  ratio compared with the non-irradiated one. It may be mentioned that Kohn, Moore and Taylor (4) had shown that irradiation effects are relatively stable in refractory oxides. The decrease in catalytic activity

of the chromic oxides as a result of both gamma and neutron irradiation , may be attributed to the decrease in the number of conduction-band electrons by the creation of chromium in interstitial positions that are not completely annihilated in the temperature range used and in the time these catalysts were working.

This work has indicated a method for introducing controlled amounts of impurities into catalysts, by neutron irradiation, that may have important practical applications.

#### ACKNOWLEDGEMENTS

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